



**People`s Democratic Republic of Algeria**  
**Ministry of Higher Education and Scientific Research**  
**University of Echahid Hamma Lakhdar - El Oued**  
**Faculty of Technology**  
**Department of Process Engineering and Petrochemicals**

**Dissertation**

ACADEMIC MASTER

**Domain:** Science and Technology

Division: Process Engineering

Specialty: Chemical engineering

**Presented by:**

Mlle. BÉLAROUCI Djihane

**Entitled:**

**Valorisation of organic waste through gasification**

Dissertation Submitted in Partial Fulfillment of the Requirements for the Master

Degree in Process Engineering

Publicly defended in: 27/05 /2025

Board of Examiners:

**Dr. AHMOUDA** Kaouthar

**Chairman**

**Dr. OUCIF KHALED** Mohammed Tayeb

**Supervisor**

**Dr. LAMI** Nassima

**Examiner**



**People`s Democratic Republic of Algeria**  
**Ministry of Higher Education and Scientific Research**  
**University of Echahid Hamma Lakhdar - El Oued**  
**Faculty of Technology**  
**Department of Process Engineering and Petrochemicals**

**Dissertation**

ACADEMIC MASTER

**Domain:** Science and Technology

Division: Process Engineering

Specialty: Chemical engineering

**Presented by:**

Mlle. BÉLAROUCI Djihane

**Entitled:**

**Valorisation of organic waste through gasification**

Dissertation Submitted in Partial Fulfillment of the Requirements for the Master

Degree in Process Engineering

Publicly defended in: 27/05 /2025

Board of Examiners:

**Dr. AHMOUDA** Kaouthar

**Chairman**

**Dr. OUCIF KHALED** Mohammed Tayeb

**Supervisor**

**Dr. LAMI** Nassima

**Examiner**

# شكر وتقدير

الحمد لله الذي بنعمته تتم الصالحات، الحمد لله الذي ألهمنا الصبر والتوفيق لإنجاز هذا العمل المتواضع.

نتوجه بجزيل الشكر إلى كل من ساعدنا من قريب أو بعيد على إنجاز هذا العمل، وفي ظل ماوجهناه من صعوبات أخص بالذكر الأستاذ المشرف الدكتور " **وصيف خالد محمد طيب** "، كما لاننسا في هذا الصدد أن نذكر جميع الأساتذة و الدكاترة على مقدمه لنا من توجيهات وإرشادات خلال هذا العمل معا تمنياتنا لهم الصحة والعافية والبركة في العمر.

وفي الأخير نسال الله تعالى بأسمائه الحسنى أن يرزقنا التوفيق جميعا وان يبلغنا جميع منازل الناجحين.



## Dedication

To my beloved parents, whose sacrifices, love, and unwavering faith in me have been the light guiding my every step.

To my dear siblings, the companions of my life journey, whose laughter, support, and encouragement made the hard days easier.

To my family and friends--those who cheered me on, lifted me up, and never let me give up--you have my heartfelt appreciation.

To everyone who offered a kind word, a helping hand, or simply believed in me when I needed it the most--thank you. And last but not least...



## **Abstract**

Gasification of organic waste represents one of the most effective valorization pathways for renewable energy and resources recovery, while this process can be affected by multi-factors like temperature, feedstock, and steam content, making the product's prediction problematic. With the popularization and promotion of artificial intelligence such as machine learning (ML), traditional artificial neural networks have been paid more attention by researchers from the data science field, which provides scientific and engineering communities with flexible and rapid prediction frameworks in the field of organic waste gasification. In this work, critical parameters including temperature, steam ratio, and feedstock during gasification of organic waste were reviewed in three scenarios including steam gasification, air gasification, and oxygen-riched gasification, and the product distribution and involved mechanism were elaborated. Moreover, we presented the details of ML methods like regression analysis, artificial neural networks, decision trees, and related methods, which are expected to revolutionize data analysis and modeling of the gasification of organic waste. Typical outputs including the syngas yield, composition, and HHVs were discussed with a better understanding of the gasification process and ML application. This review focused on the combination of gasification and ML, and it is of immediate significance for the resource and energy utilization of organic waste.

. يمثل تغويز النفايات العضوية أحد أكثر مسارات التثمين فعالية لاسترداد الطاقة المتجددة والموارد، ومع ذلك، يمكن أن يتأثر هذا العملية بعدة عوامل مثل درجة الحرارة، ونوع المادة الأولية، ومحتوى البخار، مما يجعل من الصعب التنبؤ بمنتجات العملية بدقة. ومع انتشار وتطور تقنيات الذكاء الاصطناعي مثل التعلم الآلي (ML)، بدأ الباحثون في مجال علوم البيانات يولون اهتماماً متزايداً بالشبكات العصبية الاصطناعية التقليدية، مما وفر للمجتمعين العلمي والهندسي أطر تنبؤ مرنة وسريعة في مجال تغويز النفايات العضوية.

في هذا العمل، تمت مراجعة المعلمات الحرجة مثل درجة الحرارة، ونسبة البخار، ونوع المادة الأولية أثناء تغويز النفايات العضوية في ثلاث سيناريوهات تشمل التغويز بالبخار، التغويز بالهواء، والتغويز الغني بالأوكسجين، كما تم شرح توزيع المنتجات والآليات المتضمنة. علاوة على ذلك، قمنا بعرض تفاصيل طرق التعلم الآلي مثل تحليل الانحدار، الشبكات العصبية الاصطناعية، أشجار القرار، والطرق المرتبطة بها، والتي يُتوقع أن تُحدث ثورة في تحليل البيانات ونمذجة عملية تغويز النفايات العضوية.

تمت مناقشة المخرجات النموذجية بما في ذلك إنتاج الغاز التخليقي (syngas)، وتركيبه، والقيم الحرارية العالية (HHVs) بهدف فهم أفضل لعملية التغويز وتطبيقات التعلم الآلي. يركز هذا الاستعراض على الدمج بين التغويز وتقنيات التعلم الآلي، وهو ذو أهمية مباشرة لاستغلال الموارد والطاقة من النفايات العضوية.

## FIGURES LIST

<b>Figure 1:</b> Typical gasification techniques and set including steam gasification (A), air gasification (B), and oxygen-riched gasification (C) .....	4
<b>Figure 2:</b> Influence of the steam/biomass ratio on the gas composition for the air and steam gasification of biowaste feedstock.....	31
<b>Figure 3:</b> Typical gasification mechanism from organic waste during steam gasification .....	51

## TABLES LIST

<b>Table 1:</b> Typical Calorific Values of Fuels.....	12
<b>Table 2:</b> Calorific Values of Common Fuels (Approximate):.....	13
<b>Table 3:</b> Comparison of Gasification Technologies.....	33
<b>Table 4:</b> Production Methods & Their Influence.....	36
<b>Table 5:</b> Comparison of Valorization Techniques.....	46
<b>Table 6:</b> Gasification Temperatures by Gasifier Type.....	51
<b>Table 7:</b> Comparison Table.....	53
<b>Table 8:</b> The composition of syngas depends on the production process and feedstock (coal, biomass, natural gas, waste).....	58
<b>Table 9:</b> Production Methods & Their Impact on Syngas Composition.....	59
<b>Table 10:</b> Typical Calorific Values of Common Gases.....	64
<b>Table 11:</b> Example Calculation.....	72
<b>Table 12:</b> Comparison Summary.....	82

## Summary

<b>Acknowledgments</b> .....	<b>1</b>
<b>Dedication</b> .....	<b>2</b>
<b>Abstract</b> .....	<b>3</b>
<b>FIGURES LIST</b> .....	<b>5</b>
<b>TABLES LIST</b> .....	<b>6</b>
<b>Summary</b> .....	<b>7</b>
<b>Introduction</b> .....	<b>10</b>

### Chapter I : Organic waste

<i>I.1-Sources and types of organic waste</i> .....	<b>3</b>
I.1.1.Organic waste can be categorized into several types based on its origin and composition: .....	<b>3</b>
<i>I.2 Physico-chemical Composition of Organic Waste</i> .....	<b>5</b>
I.2.1.Water Content: .....	<b>10</b>
I.2.2. Volatile matter content:.....	<b>11</b>
I.2.3.Calorific Value (Heating Value) .....	<b>11</b>
I.2.4. Elemental composition (C H O N S) .....	<b>14</b>
I.2.5.Other constituents (ashes, heavy metals) .....	<b>15</b>
<i>I.3.Variability in the Composition of Organic Waste</i> .....	<b>16</b>
I.3.1.Key Factors Affecting Variability: .....	<b>17</b>
I.3.2.Implications of Variability:.....	<b>17</b>
I.3.3.Mitigation Strategies:.....	<b>18</b>
<i>I.4.Methods for Characterizing Organic Waste</i> .....	<b>18</b>
I.4.1.Wet analysis .....	<b>20</b>
I.4.2. Spectroscopic analysis: .....	<b>22</b>
I.4.3.Thermal analysis .....	<b>25</b>

### Chapter II : Gasification of Organic Waste

<i>II.1.State of the Art in Gasification of Organic Waste</i> .....	<b>29</b>
II.1.1.Principles of gasification .....	<b>29</b>
II.1.2. Gasification technologies .....	<b>31</b>
II.1.3.Characteristics of the produced syngas .....	<b>34</b>
II.1.4.ValORIZATION of syngas .....	<b>36</b>

II.1.5.Factors influencing the gasification of organic waste .....	38
<i>II.2. Analysis of Existing Processes for the Valorization of Organic Waste .....</i>	<i>39</i>
II.2.1.Incineration.....	39
II.2.2.Composting:.....	41
II.2.3.Anaerobic Digestion.....	43
II.2.4.Pyrolysis: .....	44
<i>II.3. Comparison of Different Valorization Techniques and Selection of Gasification.....</i>	<i>45</i>
II.3.1. Comparison of Valorization Techniques.....	46
II.3.2.Selection of Gasification .....	47
II.3.3. Advantages of Gasification: .....	47
II.3.4. Challenges & Mitigation: .....	47
II.3.5. Case Studies & Applications: .....	47
II.3.6.Conclusion.....	47

### **Chapter III: The Gasifier**

<i>III.1. Choice of Gasifier and Operating Conditions .....</i>	<i>49</i>
III.1.1.Type of gasifier (fixed bed, fluidized bed, plasma, etc.).....	49
III.1.2.Gasification temperature .....	50
III.1.3.Gasifying agent (air, steam, oxygen, etc.).....	52
III.1.4.Gasification flow rate .....	54
III.1.5.Ratio of gasifying agent to waste .....	55
<i>III.2.Implementation of Gasification Experiments.....</i>	<i>56</i>
III.2.1. Experimental Setup Components.....	56
III.2.2.Key Experimental Parameters .....	56
III.2.3.Measurement and Analysis Techniques.....	57
III.2.4. Safety Considerations.....	57
III.2.5. Data Processing and Analysis .....	58
<i>III.3. Analysis of Produced Syngas .....</i>	<i>58</i>
III.3.1 Analysis of Produced Syngas.....	58
III.3.2.Pollutant gas content (HCl, SO <sub>2</sub> , NO <sub>x</sub> , etc.) .....	62
<i>III.4. Analysis of Residual Ashes .....</i>	<i>64</i>
III.4.1.Chemical composition of ashes.....	64
III.4.2.Morphological characterization of ashes.....	67
<i>III.5. Material and Energy Balance of Gasification.....</i>	<i>68</i>
III.5.1.Material Balance .....	68
III.5.2.Energy Balance .....	69

## **Chapter IV: Economic and Environmental Aspects of Valorizing Organic Waste through Gasification.**

<i>IV.1. Cost Analysis of the Gasification Process</i> .....	72
IV.1.1. Initial investment.....	72
IV.1.2. Operating costs.....	73
IV.1.3. Revenues from the sale of energy or chemical products .....	75
<i>IV.2. Environmental Impact Analysis of the Gasification Process</i> .....	77
IV.2.1. Greenhouse gas emissions .....	77
IV.2.2. Pollutant releases into air, water, and soil.....	78
IV.2.3. Comparison with other organic waste valorization processes .....	80
<b>Conclusion</b> .....	<b>83</b>
<b>References</b> .....	<b>86</b>

# **Introduction**

### **Introduction**

The management of organic waste has become a critical environmental and economic issue, particularly in developing countries where organic materials constitute a major portion of municipal solid waste. Inadequate disposal practices, such as open dumping and landfilling, result in serious consequences including greenhouse gas emissions, water and soil contamination, and the depletion of available landfill space. These practices are not only unsustainable but also represent a lost opportunity to harness the value embedded in organic waste.

Organic waste, if treated properly, can be a significant resource. Through techniques like gasification and pyrolysis, it is possible to convert biodegradable materials—such as food scraps, agricultural residues, and garden waste—into valuable energy carriers such as syngas, bio-oil, and biochar. These processes contribute to clean energy generation, pollution reduction, and the promotion of circular economy principles by transforming waste into useful products.

However, the path toward effective valorization of organic waste through advanced thermochemical conversion technologies is hindered by multiple barriers. These include a lack of infrastructure, limited public awareness, insufficient governmental support, and economic constraints. In developing countries, these challenges are further compounded by weak institutional frameworks and a lack of stakeholder coordination.

This thesis is structured into several chapters. Chapter One, titled "General Overview", introduces the research problem and provides essential background information. Chapter Two, "Literature Review", presents previous studies and theoretical concepts related to the topic. Chapter Three, "Materials and Methods", describes the methodology, tools, and procedures used in the research. Chapter Four, "Results and Discussion", analyzes the obtained results and discusses their implications. Finally, the thesis ends with a General Conclusion that summarizes the main findings and offers recommendations for future research.

# **Chapter I**

## **Organic waste**

Organic waste, comprising biodegradable materials such as food scraps, garden trimmings, agricultural residues, and paper products, has become a central concern in global waste management strategies. Its rising volume, driven by rapid urbanization, population growth, and consumption habits, presents both environmental risks and opportunities for sustainable development. While often discarded, organic waste holds valuable potential when treated properly—serving as a source for compost, energy, and bio-based products. This chapter provides an overview of the main sources, types, and characteristics of organic waste, emphasizing how understanding its composition is essential for choosing appropriate valorization techniques.

### **I.1-Sources and types of organic waste**

Organic waste originates from a wide range of sources and consists primarily of biodegradable materials. Its composition varies depending on the origin, but it typically includes food scraps, plant residues, paper products, and other decomposable materials. The most common sources of organic waste include households, agricultural activities, food processing industries, public institutions, and commercial establishments such as markets and restaurants.

In residential areas, organic waste often comes from kitchen activities—vegetable peels, leftover food, coffee grounds, eggshells, and garden clippings. Agricultural operations contribute significantly through crop residues, animal manure, and spoiled produce. The food industry generates large volumes of organic by-products during processing, packaging, and distribution. Markets and restaurants also discard a notable amount of organic material that is no longer suitable for consumption.

#### **I.1.1.Organic waste can be categorized into several types based on its origin and composition:**

-Food Waste – Includes raw and cooked food leftovers, fruit and vegetable peels, dairy, and bakery waste.

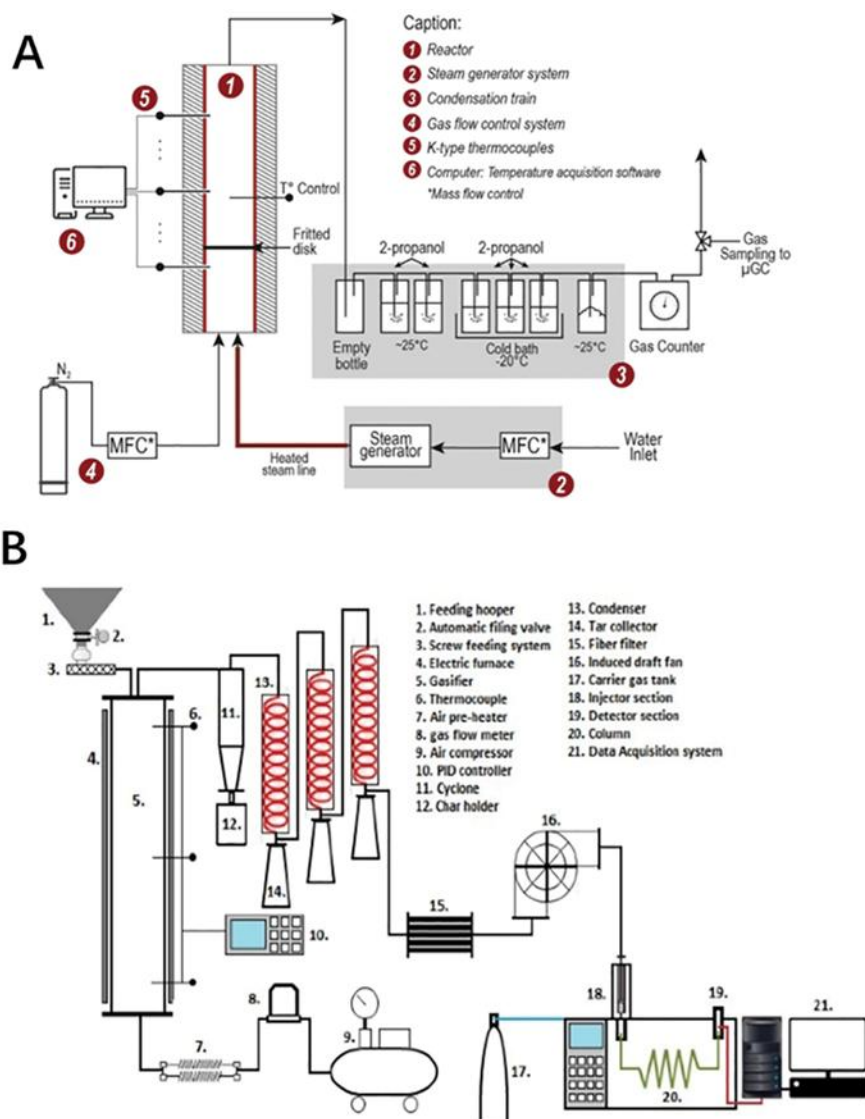
-Green Waste – Consists of yard trimmings, grass clippings, leaves, and garden debris.

-Agricultural Waste – Covers crop stalks, husks, shells, and animal waste from farms.

-Paper-Based Waste – Uncoated paper, cardboard, and similar cellulose-rich biodegradable materials.

-Wood Waste – Sawdust, untreated wood shavings, and timber offcuts.

-Market and Slaughterhouse Waste – Organic remains of fruits, vegetables, and animal products.



**Figure 1:** Typical gasification techniques and set including steam gasification (A), air gasification (B), and oxygen-riched gasification (C)

Each type has unique characteristics in terms of moisture content, nutrient value, and decomposition rate. Understanding the diversity of organic waste sources and types is essential for choosing suitable treatment techniques such as composting, anaerobic digestion, or gasification. Effective segregation and categorization at the source can

---

enhance the efficiency of resource recovery and reduce the environmental burden of waste disposal.

## **I.2 Physico-chemical Composition of Organic Waste**

Composting relies on the natural process of decomposition of organic wastes by microorganisms under controlled conditions to produce an end-product with significant bioenergy potential and nutritional value [1]. It is associated to multiple environmental, social, and economical benefits including sanitation, bioremediation and waste management. For years and still nowadays, organic waste is considered as a serious environmental issue especially with the exponential population growth and the increased rate of per capita food consumption that contributes directly to the increase generation of waste. Food waste are usually disposed in landfills or incinerators which are environmentally, socially, and economically undesirable techniques that require both energy and space. In addition, they liberate unpleasant odours, lead to greenhouse gas emissions and pollute surrounding soils, groundwater and water bodies [2,3]. The possibility to dispose organic waste by using them as materials for compost preparation is seen as a key solution to alleviate the burden on the environment. In addition, composting plays an important role in sustaining soil fertility. It improves soil aggregation, infiltration and aeration and increases water holding capacity allowing therefore the soil to become more resistant to drought, diseases and toxicity. Furthermore, it improves the nutrient content and microbial activity in soil and helps in the elimination of weed and pests [4,5]. These benefits manifest themselves in reducing cropping risks, higher crop yields and lowering outlays on inorganic fertilizers [6,7].

Different types of composting techniques, such as cold composting, vermicomposting, Bokashi composting, or hot aerated composting can be applied in small or large scales. Cold composting involves decomposition of organic materials in nature for example a fallen tree in the forest. Generally, the leaves are first decomposed by bacteria and the moist punky wood of the trunk is attacked by fungi and some bacteria and insects. In vermicomposting, worms attack the organic matter to break it down into a high value compost. Anaerobic degradation of organic waste, or Bokashi composting, is another process that uses a specific group of microorganisms to ferment organic matter in absence of oxygen in an acidic environment, resulting in a finished product that can be easily

---

digested by the soil biota [8]. The hot aerated composting technique begins with the proper balance of organic material and appropriate amount of water and air in a pile of adequate size which goes through three phases: the heating up or mesophilic phase, the hot or thermophilic phase and the curing or maturation phase. The pile includes organic matter that may be classified as green and brown materials. The brown materials, such as wood chips or fallen leaves, are high in carbon and represent a source of energy for the composting microbes. Green materials such as grass clippings, fruit and vegetable peels are a source of nitrogen. Understanding the Carbon to Nitrogen ratio of the pile is very important because it is very effective in creating a hot compost pile with minimum odour. The ideal C: N ratio of a compost pile is 25:1 to 30:1. If the ratio is too low the pile may get excessively hot or the pile uses all the oxygen in it and turns into an anaerobic process. This technique is a common practice for large scale composting in which waste are formed into rows of long piles and aerated by turning the pile either by mechanical or manual means. In-vessel aerobic composting is a method of composting in which waste are placed in a rotary drum. Rotating causes, the material to tumble and this provides good distribution of the organic matter [9]. The hot aerated composting technique is applied too in small scales at home or in schools, universities and hospitals where the composting process is used to treat aerobically small amount of biodegradable waste without referring to automation methods.

Decomposition of organic waste, following the hot aerated composting technique, starts with the breaking down of large organic materials in the compost bin by small insects and bugs like beetles, centipedes, mites, earthworms, ants. Then comes the role of bacteria and fungi for a further decomposition of the compost matter and liberation of nutrients. Microbial diversity is important at that step because each microorganism produces specific sets of enzymes to degrade certain organic molecules [10]. *Firmicutes* were found in the early stages of the composting. *Actinomycetes*, members of the Phylum *Actinobacteriota*, are characterized by their ability to decompose complex compounds such as proteins, cellulose, and lignin [11]. *Proteobacteria* are gram negative bacteria that include gamma-proteobacteria, reproducing in temperature ranging from  $-10\text{ }^{\circ}\text{C}$  to  $40\text{ }^{\circ}\text{C}$ , beta-proteobacteria capable of increasing the availability of nitrogen in the soil and ammonia oxidizing bacteria helping in the oxidation of ammonia to nitrite [12,13].

The quality of compost relies on its microbial population but also on several other factors including its water retention ability and its content in organic matter, a valuable

---

component of the compost for the soil health improvement. Compost pH may also affect plant growth and should be preferably moderately acidic to moderately basic, that means between pH 6 to 8. Manure based composts, with a slightly basic pH, are unsuitable for acid loving plants such as Rhododendron and Blueberry [14]. Electrical Conductivity, an indicator of soluble salt content, must be preferably low. Macro-nutrients such as nitrogen, phosphorous and potassium are important for plant nutrition.

In this study we analysed twelve compost samples by investigating their physicochemical properties (Organic matter content, nitrogen, potassium, phosphorous, sodium, water retention, electrical conductivity, pH) and by studying their microbial composition using 16S rRNA metagenomics sequencing technique targeting v3-v4 regions with Illumina MiSeq. Learning more about these properties will help in understanding better the degradation process and in improving the composting technique.

#### **-Methods:**

This is an analytical experimental study that involved the assessment of the physicochemical properties and the microbiological composition of twelve different compost preparations performed by Zayed University students on Dubai Campus between September 2018 and January 2019.

#### **-Composting technique:**

All compost samples were prepared on Zayed University campus in Dubai, using the hot aerobic method, and were mainly composed of common organic wastes which fall into two categories green and brown materials in 1:3 ratios. The green materials used were grass clippings, green leaves, flowers, hair, herbs, fruit and vegetable peels. Brown materials consisted of fallen leaves, cardboard, paper, hay, corn cobs, pine needles, crushed egg shells, tea leaves, old herbs, spices and cereals. Coffee grounds were added as activators to accelerate the composting process to the samples 1, 2, 4, 6, 7, 8, and 11. Some of the food items like citrus peels, onion were excluded because of their acidic or antimicrobial properties. Dairy or meat products were not added to prevent bad odours and attraction of rodents. Heavily coated or printed paper and diseased plants were not used because of toxicity. All composts were prepared in wooden box chambers with the dimension of 1 m × 1 m × 1 m. Wooden boxes were not tightly sealed to facilitate aeration and compost preparations were mixed and watered once every week for 12 weeks.

---

### - Physicochemical characteristics

At the end of the 12 weeks, 2 kg of each compost preparation were dried in the laboratory oven at 60 °C for 12 h, slightly ground to finer particles using a large brass mortar and pestle, then sieved with a 2 mm equipment.

To check the presence of organic matter in each preparation, 10 g of compost was put in a crucible and kept in the furnace at 550 °C for 4 h and allowed to cool; then the final weight was noted.

Moisture content or water retention was measured using a soil moisture unit with a pressure of 0.1 Bar. Each sample was put in a dish filled with distilled water until the sample is moist, then the instrument was turned on. Once the pressure instrument stopped, the weight of the dish containing the fresh sample was recorded. Then, the sample was dried in the laboratory's oven at 100 °C for 12 h and cooled down. The weight of the dry sample was taken, and the water retention percentage of each sample was calculated using the average of replicates.

Electrical conductivity (EC) and pH values were measured using respectively an electrical conductivity meter and a pH meter. Each sample was diluted in a ratio of 1:5 with distilled water, stirred and allowed to settle overnight before getting the readings.

Kjeldahl total Nitrogen was calculated using the Kjeldahl method which consists of two main steps, digestion and distillation. A total of 0.5 g of dried sample was digested with half Kjeldahl tablet, 1 ml distilled water and 20 ml sulphuric acid in the digestion tube at 150 °C for 2 h. Later the sample was distilled with 25 ml boric acid. After complete distillation, the colour of the distillate changes from pink to different shades of green depending on the amount of nitrogen. This was titrated against 0.01 N sulphuric acid. Readings were noted to calculate the available nitrogen content in the samples.

To assess the assimilable concentrations of phosphorous (P), sodium (Na) and potassium (K), compost samples were digested using acid mixtures (H<sub>2</sub>SO<sub>4</sub>, HCl, and Ammonium) and subjected to colorimetric analysis after filtration. The standards for P, Na and K were prepared to design standard curves. A total of 5 ml of digested samples were added to volumetric flasks with 10 ml of 2 N Nitric Acid and treated with Molybdate-Vanadate for 20 min. Phosphorous content was measured using a UV-VIS Scanning spectrophotometer Spectro UV-2510TS. To measure the Na and K, the samples were

diluted 10 times and the readings were taken using a flame photometer. The readings were then compared with standards and calculated the amount of sodium, potassium and phosphorous present in the sample. The carbon content was calculated using the formula [Organic matter (%) = Total organic carbon (%) x 1.72]. The number 1.72 is the commonly used conversion factor which provides a reasonable estimate and is suitable for most of the soil type [16].

- Microbial identification using 16S rRNA metagenomics study
- Extraction of genomic DNA and 16S rRNA Illumina sequencing

Microbial DNA were extracted from samples using the ZymoBIOMICS™ DNA Miniprep Kit (Zymo Research Corporation, California, USA), following the manufacturer's instructions and assessed for quality using the DeNovix dsDNA High Sensitivity Fluorescent Assay Kit and measured on the DeNovix DS-11 FX spectrophotometer/fluorometer (DeNovix Inc., Delaware, USA). The DNA integrity was checked using agarose gel electrophoresis.

Amplicon libraries of the v3 and v4 regions were generated using two-step Polymerase Chain Reaction (PCR) process followed to generate barcoded amplicons from v3-v4 region of 16S rRNA genes. First round PCR has performed with 1  $\mu$ M of 16S Amplicon PCR Forward Primer (5'

TCGTCGGCAGCGTCAGATGTGTATAAGAGACAGCCTACGGGNGGCWGCAG) and Reverse Primer (5'

GTCTCGTGGGCTCGGAGATGTGTATAAGAGACAGGACTACHVGGGTATCTAATCC). Later purified this using AMPure XP beads (Beckman Coulter, California, USA) and used for the second round PCR along with sample-specific barcodes (Nextera XT index kit, Illumina). Final libraries were quantified, using DeNovix dsDNA High Sensitivity Fluorescent Assay Kit. Subsequently, they were normalized, multiplexed and sequenced using Illumina MiSeq with a paired-end protocol (2  $\times$  300 bp).

### **-Bioinformatics and statistical analysis**

The sequencing run was analysed with the QIIME 2 with demultiplexing. The raw sequence data in the *fastq* files were processed to remove Illumina adaptors, low-quality and chimeric regions. The processed sequence data were then assessed for the analysis.

The DADA2 pipeline was used for detecting and correcting Illumina amplicon sequence data. Quality filtered reads were assigned to OTUs applying the open-reference OTU picking protocol using QIIME toolkit. Taxonomic analysis was performed using average taxonomic composition of the 12 samples. The *qiime2* feature-classifier trained on the SILVA 138 reference was used to classify ASVs at different taxonomical levels (7 levels: Kingdom; Phylum; Class; Order; Family; Genus; Species).

### **I.2.1. Water Content:**

Water Content refers to the amount of water present in a substance, such as soil, food, air, or biological materials. It is a crucial parameter in various fields, including agriculture, engineering, food science, and environmental studies.

-Types of Water Content Measurement:

1. Gravimetric Water Content ( $\theta_g$ )
2. Measured by weighing a sample before and after drying.

- Where:

-  $(W_{\text{wet}})$  = Wet weight of the sample

-  $(W_{\text{dry}})$  = Dry weight (after oven-drying)

-Volumetric Water Content ( $\theta_v$ ) – Measures the volume of water relative to the total volume of the sample.

-Relative Humidity (RH)

– Indicates moisture content in air or gases.

Importance of Water Content:

-Agriculture: Determines irrigation needs and soil health.

-Food Industry: Affects shelf life, texture, and quality.

-Construction: Influences soil compaction and stability.

-Environmental Science: Helps in studying groundwater and ecosystem health.

## **I.2.2. Volatile matter content:**

### **I.2.2.1. Volatile Matter Content in Coal and Other Materials**

#### **Definition:**

Volatile matter (VM) refers to the components of a material (such as coal, biomass, or petroleum) that are released as gases when the material is heated in the absence of air (pyrolysis). It consists of hydrocarbons, carbon monoxide, carbon dioxide, hydrogen, and other gases.

### **I.2.2.2. Importance of Volatile Matter Content**

1. **Coal Classification:** VM is a key parameter in coal ranking (e.g., lignite, bituminous, anthracite).

2. **Combustion & Gasification:** Higher VM content improves ignition but may lead to higher emissions.

3. **Coke Production:** Low VM is preferred for metallurgical coke.

4. **Biomass & Waste:** Influences energy yield and combustion behavior.

### **I.2.2.3. Measurement Standards (ASTM & ISO)**

- **ASTM D3175-20:** Standard Test Method for Volatile Matter in Coal.
- **ISO 562:2010:** Hard coal and coke – Determination of volatile matter.
- **ISO 18123:2015:** Solid biofuels – Determination of volatile matter.

## **I.2.3. Calorific Value (Heating Value)**

#### **Definition:**

The **calorific value (CV)** of a fuel is the amount of heat energy released per unit mass (or volume) during complete combustion. It is a critical parameter for assessing fuel quality and energy efficiency.

### **I.2.3.1. Types of Calorific Value**

#### **I.2.3.1.a. Gross Calorific Value (GCV) / Higher Heating Value (HHV):**

○ Total heat released, including the latent heat of vaporization of water in combustion products.

○ Measured using a bomb calorimeter.

#### **I.2.3.1.b. Net Calorific Value (NCV) / Lower Heating Value (LHV):**

○ Excludes the latent heat of vaporization (water remains as vapor).

○ More practical for industrial applications.

○ **NCV  $\approx$  GCV – (Latent heat of water vapor formed)**

#### **I.2.3.1.c. Measurement Standards (ASTM, ISO, DIN)**

• **ASTM D5865-19:** Standard Test Method for Gross Calorific Value of Coal and Coke.

• **ISO 1928:2009:** Solid mineral fuels – Determination of gross calorific value.

• **DIN 51900:** Testing of solid and liquid fuels – Determination of calorific value.

**Table 1:** Typical Calorific Values of Fuels

<b>Fuel Type</b>	<b>Gross Calorific Value (MJ/kg)</b>	<b>Net Calorific Value (MJ/kg)</b>
Anthracite Coal	30–35	28–33
Bituminous Coal	24–30	22–28
Sub-bituminous	18–24	17–22
Lignite	15–18	14–17
Wood (Dry)	16–20	14–18
Diesel	45–46	42–44
Natural Gas	50–55 (MJ/m <sup>3</sup> )	45–50 (MJ/m <sup>3</sup> )

#### **I.2.3.2. Calorific value**

The **calorific value** (also called **heating value** or **energy value**) is the amount of heat energy released when a fuel or food is completely burned. It is typically measured in units like **joules per gram (J/g)**, **kilojoules per gram (kJ/g)**, **calories per gram (cal/g)**, or **British Thermal Units per pound (BTU/lb)**.

#### **Types of Calorific Value:**

##### **1. Higher Calorific Value (HCV) / Gross Calorific Value (GCV):**

- Total heat energy released when a fuel is burned, including the heat recovered by condensing water vapor in the exhaust gases.
- Measured in a bomb calorimeter.

##### **2. Lower Calorific Value (LCV) / Net Calorific Value (NCV):**

- Heat energy available after subtracting the energy lost due to water vapor in exhaust gases.
- More practical for real-world applications since exhaust gases usually escape as vapor.

**Table 2:** Calorific Values of Common Fuels (Approximate):

<b>Fuel Type</b>	<b>Gross Calorific Value (MJ/kg)</b>
Gasoline	45–46
Diesel	44–45
Natural Gas (Methane)	50–55
Coal (Bituminous)	24–35
Wood (Dry)	16–21
Hydrogen	142

Calorific Value in Food:

- Measured in kilocalories (kcal) or kilojoules (kJ) per gram.
- Carbohydrates: ~4 kcal/g (~17 kJ/g)
- Proteins: ~4 kcal/g (~17 kJ/g)
- Fats: ~9 kcal/g (~37 kJ/g)
- Alcohol (Ethanol): ~7 kcal/g (~29 kJ/g)

Measurement Methods:

- Bomb Calorimeter (for fuels and food) – Measures heat released under controlled conditions.
- Gas Chromatography (for gaseous fuels).

#### **I.2.4. Elemental composition (C H O N S)**

The elemental composition **C, H, O, N, S** refers to the five key elements commonly found in organic compounds, particularly in biological molecules. Here's a breakdown of their roles and occurrences:

##### **I.2.4.1. Carbon (C)**

- **Role:** Backbone of organic molecules, forms covalent bonds with other elements.
- **Found in:** All organic compounds (e.g., carbohydrates, lipids, proteins, nucleic acids).

##### **I.2.4.2. Hydrogen (H)**

- **Role:** Bonds with carbon and oxygen, contributes to acidity/basicity.
- **Found in:** Almost all organic molecules (e.g., water, hydrocarbons, biomolecules).

##### **I.2.4.3. Oxygen (O)**

- **Role:** Key in energy metabolism (respiration), forms polar bonds (hydroxyl, carbonyl groups).
- **Found in:** Water, carbohydrates, proteins, lipids, nucleic acids.

##### **I.2.4.4. Nitrogen (N)**

- Role: Essential for amino acids (proteins), nucleic acids (DNA/RNA), and some coenzymes.

- Found in: Proteins (amines, amides), nucleotides (purines, pyrimidines).

#### **I.2.4.5.Sulfur (S)**

- Role: Stabilizes protein structures (disulfide bonds in cysteine), found in coenzymes.

- Found in: Amino acids (methionine, cysteine), vitamins (biotin, thiamine), some antibiotics.

#### **I.2.4.6.Common Compounds with C, H, O, N, S:**

- Proteins (e.g., enzymes, antibodies) – Contain C, H, O, N, S.

- DNA/RNA – Primarily C, H, O, N, P (sulfur appears in some nucleobases).

- Coenzymes (e.g., Coenzyme A) – Contains S.

- Fossil fuels (e.g., coal, crude oil) – Often contain traces of N, S.

#### **I.2.4.7.Analytical Techniques for CHONS Composition:**

- Elemental Analysis (EA): Measures % composition of C, H, N, S, O.

- Mass Spectrometry (MS): Detects molecular weight and elemental isotopes.

- X-ray Photoelectron Spectroscopy (XPS): Surface elemental analysis.

#### **I.2.5.Other constituents (ashes, heavy metals)**

The term "**other constituents (ashes, heavy metals)**" typically refers to non-fuel components found in coal, biomass, waste materials, or other combustible substances. These can impact combustion efficiency, emissions, and environmental safety. Here's a breakdown:

##### **I.2.5.1.Ashes**

- Composition: Primarily inorganic minerals like silica ( $\text{SiO}_2$ ), alumina ( $\text{Al}_2\text{O}_3$ ), iron oxide ( $\text{Fe}_2\text{O}_3$ ), calcium oxide ( $\text{CaO}$ ), and magnesium oxide ( $\text{MgO}$ ).

- Sources: Naturally present in coal, biomass, or introduced during processing.

- Effects:
  - Reduces combustion efficiency (non-combustible material).
  - Can cause slagging (deposits in boilers) and fouling (corrosion).
  - Requires disposal (landfill or recycling in construction materials).

### **I.2.5.2. Heavy Metals**

- Common Heavy Metals in Fuels:
  - Mercury (Hg) – Highly toxic, volatile, and hard to capture.
  - Lead (Pb), Cadmium (Cd), Arsenic (As) – Carcinogenic, harmful to ecosystems.
  - Chromium (Cr), Nickel (Ni) – Can be toxic in certain forms.
- Sources: Naturally occurring in coal, industrial waste, or contaminated biomass.
- Effects:
  - Air Pollution: Emitted as fine particulate matter (PM<sub>2.5</sub>) or vapors.
  - Soil & Water Contamination: Leaches from ash disposal sites.
  - Health Risks: Bioaccumulation in food chains, causing neurological and organ damage.

### **I.2.5.3. Environmental & Regulatory Concerns**

- Emission Controls: Scrubbers, electrostatic precipitators, and activated carbon injection (for Hg).
- Ash Management: Safe disposal or reuse (e.g., in cement production).
- Regulations:
  - Coal Combustion Residuals (CCR) Rule (EPA, USA) for ash disposal.
  - Mercury and Air Toxics Standards (MATS) limiting heavy metal emissions.

## **I.3. Variability in the Composition of Organic Waste**

Variability in the composition of organic waste is a significant challenge for waste management, recycling, and energy recovery processes. Organic waste includes a wide

---

range of biodegradable materials, such as food scraps, yard waste, agricultural residues, and animal manure. The composition can vary due to several factors:

### **I.3.1.Key Factors Affecting Variability:**

#### **I.3.1.1.Source of Waste**

- Municipal Solid Waste (MSW): Household food waste, garden trimmings.
- Agricultural Waste: Crop residues, spoiled produce, manure.
- Industrial/Commercial Waste: Food processing byproducts, restaurant waste.
- Sewage Sludge: Organic matter from wastewater treatment.

#### **I.3.1.2.Seasonal Variations**

- Higher fruit/vegetable waste in summer, more yard waste in autumn.
- Festive seasons may increase food waste (e.g., holidays, weddings).

#### **I.3.1.3.Geographical & Cultural Differences**

- Diets influence food waste composition (e.g., more rice waste in Asia, bread waste in Europe).
- Urban vs. rural waste (more packaged food waste in cities).

#### **I.3.1.4.Collection & Segregation Practices**

- Poor segregation leads to contamination (plastics, glass mixed with organics).
- Source-separated organic waste is more homogeneous.

#### **I.3.1.5.Degradation State**

- Fresh waste vs. partially decomposed waste affects moisture content and nutrient levels.

### **I.3.2.Implications of Variability:**

- Biogas Production: High moisture & fats improve anaerobic digestion but may cause operational issues.
- Composting: Carbon-to-nitrogen (C/N) ratio affects decomposition speed and quality.
- Waste-to-Energy: Inconsistent calorific value affects incineration efficiency.
- Policy & Recycling Targets: Variability complicates standardization in waste treatment.

### **I.3.3.Mitigation Strategies:**

- Improved Sorting & Pre-treatment (shredding, dewatering).
- Feedstock Blending (mixing different wastes to balance C/N ratio).
- Real-time Monitoring (sensors for moisture, pH, organic content).
- Public Awareness & Source Separation to reduce contamination.

### **I.4.Methods for Characterizing Organic Waste**

Characterizing organic waste is essential for understanding its composition, behavior, and potential applications in recycling, composting, energy production, and waste management. Below are key methods used for characterizing organic waste:

#### **1. Physical Characterization**

- Moisture Content: Measured by drying a sample at 105°C until constant weight (gravimetric method).
- Bulk Density: Determined by measuring the mass per unit volume (kg/m<sup>3</sup>).
- Particle Size Distribution: Sieve analysis or laser diffraction for assessing particle sizes.
- Porosity & Water Holding Capacity: Important for composting and soil amendment applications.

#### **2. Chemical Characterization**

- Proximate Analysis:

- Volatile Solids (VS): Indicates organic content (measured by loss on ignition at 550°C).
- Fixed Carbon & Ash Content: Residual inorganic matter after combustion.
- Ultimate Analysis (Elemental Composition):
  - Carbon (C), Hydrogen (H), Nitrogen (N), Sulfur (S), Oxygen (O) via CHNS/O analyzers.
- pH & Electrical Conductivity (EC): Affects microbial activity in composting.
- Total Organic Carbon (TOC) & Chemical Oxygen Demand (COD): Measures organic load.
- Biochemical Methane Potential (BMP): Assesses biogas yield potential.
- Nutrient Content (N, P, K): Important for compost quality.
- C/N Ratio: Critical for composting efficiency (optimal range: 25-30:1).
- Heavy Metals & Contaminants: ICP-MS or AAS for detecting Pb, Cd, Hg, etc.

### **3. Biological Characterization**

- Biodegradability Tests:
  - Aerobic Respiration (AT4, SOUR): Measures oxygen consumption.
  - Anaerobic Digestion Tests: Determines biogas/methane yield.
- Microbial Community Analysis (DNA sequencing, qPCR): Identifies key decomposers.
- Enzymatic Activity: Tests for cellulase, protease, lipase activity.

### **4. Thermal Characterization**

- Calorific Value (Higher Heating Value - HHV): Measures energy content via bomb calorimeter.
- Thermogravimetric Analysis (TGA): Decomposition behavior under heating.
- Differential Scanning Calorimetry (DSC): Heat flow during thermal degradation.

### **5. Spectroscopic & Chromatographic Methods**

- Fourier Transform Infrared Spectroscopy (FTIR): Identifies functional groups (e.g., lignin, cellulose).
- Nuclear Magnetic Resonance (NMR): Analyzes molecular structure.
- Gas Chromatography-Mass Spectrometry (GC-MS): Detects volatile organic compounds (VOCs).
- High-Performance Liquid Chromatography (HPLC): Quantifies sugars, organic acids, phenols.

## 6. Advanced Characterization

- X-ray Diffraction (XRD): Identifies crystalline compounds (e.g., minerals in ash).
- Scanning Electron Microscopy (SEM): Examines surface morphology.
- Stable Isotope Analysis ( $\delta^{13}\text{C}$ ,  $\delta^{15}\text{N}$ ): Tracks organic matter sources.

### Applications of Characterization Data

- Waste-to-Energy (WtE): Suitability for incineration, gasification, or anaerobic digestion.
- Composting Optimization: Adjusting C/N ratio, moisture, and aeration.
- Regulatory Compliance: Ensuring safe levels of contaminants.
- Material Recovery: Extracting valuable compounds (e.g., bio-based chemicals).

### I.4.1. Wet analysis

Wet analysis refers to a set of laboratory techniques used in chemistry to identify or quantify the components of a substance through liquid-phase reactions. Unlike instrumental or "dry" methods (e.g., spectroscopy, chromatography), wet analysis relies on traditional chemical reactions, titrations, precipitations, or extractions performed in solution.

#### I.4.1.1. Key Features of Wet Analysis:

1. **Sample Preparation:** The sample is often dissolved in a solvent (e.g., water, acid, or organic liquid).

2. **Chemical Reactions:** Reactions like acid-base neutralization, redox, or complexation are used.

3. **Observation:** Changes (color, precipitate formation, gas evolution) are monitored.

4. **Quantitative/Qualitative:** Can determine concentration (e.g., titration) or identify components (e.g., spot tests).

#### **I.4.1.2. Common Wet Analysis Techniques:**

##### 1. Titration (Volumetric Analysis):

- Acid-Base Titration: Determines concentration using pH indicators.
- Redox Titration: Measures oxidizing/reducing agents (e.g., permanganometry).
- Complexometric Titration: Uses chelating agents like EDTA.

##### 2. Gravimetric Analysis:

- A component is precipitated, filtered, dried, and weighed (e.g., sulfate as  $\text{BaSO}_4$ ).

##### 3. Colorimetric Analysis:

○ Concentration is determined by comparing solution color intensity (e.g., using a spectrophotometer).

##### 4. Spot Tests:

- Quick qualitative tests (e.g., flame tests for metals, iodide-starch for oxidizers).

#### **I.4.1.3. Advantages:**

- Low cost (minimal equipment needed).
- High accuracy for certain applications (e.g., titrations).
- Versatile for both organic and inorganic samples.

#### **I.4.1.4. Disadvantages:**

- Time-consuming compared to instrumental methods.
- Requires skilled technicians.

- May use hazardous reagents.

#### **I.4.1.5.Applications:**

- Environmental testing (water hardness, pollutant levels).
- Pharmaceutical quality control.
- Food industry (nutrient analysis).
- Metallurgy (ore composition).

#### **I.4.1.6.Example:**

To determine the chloride concentration in water:

1. Add silver nitrate ( $\text{AgNO}_3$ ) to the sample.
2. Observe white precipitate ( $\text{AgCl}$ ).
3. Filter, dry, and weigh the precipitate (gravimetric), or titrate with thiocyanate (volumetric).

Wet analysis remains fundamental in labs where precision is critical or where advanced instruments are unavailable. However, it's often supplemented or replaced by faster instrumental methods in modern settings.

### **I.4.2. Spectroscopic analysis:**

Spectroscopic analysis is a broad field of study that involves the interaction of matter with electromagnetic radiation to obtain information about the composition, structure, and properties of materials. It is widely used in chemistry, physics, astronomy, biology, and environmental science. Here's an overview of key concepts and techniques:

#### **I.4.2.1. Basic Principles**

Spectroscopy measures how matter absorbs, emits, or scatters light (or other electromagnetic radiation) at different wavelengths. The resulting spectra provide details about:

- Atomic and molecular structure
- Chemical composition

- Concentration of substances
- Dynamic processes (e.g., reaction kinetics)

#### **I.4.2.2. Types of Spectroscopy**

Spectroscopic techniques are categorized based on the type of radiation-matter interaction:

##### **A. Absorption Spectroscopy**

Measures how much light a sample absorbs at different wavelengths.

- UV-Vis Spectroscopy: Analyzes electronic transitions (useful for organic compounds, transition metals).
- Infrared (IR) Spectroscopy: Studies molecular vibrations (identifies functional groups).
- Atomic Absorption Spectroscopy (AAS): Quantifies metal concentrations.
- X-ray Absorption Spectroscopy (XAS): Probes electronic and structural properties.

##### **B. Emission Spectroscopy**

Measures light emitted by excited atoms or molecules.

- Atomic Emission Spectroscopy (AES): Used in elemental analysis (e.g., inductively coupled plasma (ICP-AES)).
- Fluorescence & Phosphorescence Spectroscopy: Detects emitted light after excitation (used in biochemistry, materials science).

##### **C. Scattering & Reflection Spectroscopy**

- Raman Spectroscopy: Measures inelastic scattering of light (complements IR spectroscopy).
- X-ray Diffraction (XRD): Analyzes crystal structures.
- Ellipsometry: Studies thin films via reflected light.

##### **D. Magnetic Resonance Spectroscopy**

---

- Nuclear Magnetic Resonance (NMR): Examines nuclear spin transitions (for molecular structure determination).

- Electron Paramagnetic Resonance (EPR): Studies unpaired electrons (free radicals, transition metals).

#### E. Mass Spectrometry (MS)

While not strictly spectroscopy, MS is often coupled with spectroscopic techniques to analyze mass-to-charge ratios of ions.

#### **I.4.2.3.Applications**

- Chemistry: Identifying unknown compounds, studying reaction mechanisms.
- Biology & Medicine: Protein structure (NMR), DNA sequencing (fluorescence), medical diagnostics (MRI).
- Environmental Science: Detecting pollutants (AAS, ICP-MS).
- Astronomy: Analyzing stellar composition via light spectra.
- Materials Science: Characterizing nanomaterials, polymers, and semiconductors.

#### **I.4.2.4.Instrumentation**

Common components of spectroscopic instruments include:

- Light source (e.g., laser, lamp).
- Monochromator or interferometer (to select wavelengths).
- Sample holder (cuvette, pellet, or vacuum chamber).
- Detector (photodiode, CCD, PMT).
- Data processor (software for spectral analysis).

#### **I.4.2.5. Data Interpretation**

- Peak positions indicate types of bonds or elements.
- Peak intensities relate to concentration (Beer-Lambert law in absorption spectroscopy).

- Spectral fingerprints help identify unknown substances.

#### **I.4.2.6. Advanced Techniques**

- Time-Resolved Spectroscopy: Studies fast processes (e.g., femtosecond laser spectroscopy).
- Hyperspectral Imaging: Combines spectroscopy with imaging for spatial analysis.
- Terahertz Spectroscopy: Probes intermolecular interactions.

#### **I.4.3. Thermal analysis**

Thermal analysis refers to a group of techniques used to study the properties of materials as they change with temperature. These methods are widely used in materials science, chemistry, pharmaceuticals, and engineering to characterize phase transitions, thermal stability, composition, and other thermodynamic properties.

##### **I.4.3.1. Common Thermal Analysis Techniques:**

1. Differential Scanning Calorimetry (DSC)
  - Measures heat flow into or out of a sample as a function of temperature or time.
  - Applications: Melting points, glass transitions, crystallization, curing reactions, and specific heat capacity.
2. Thermogravimetric Analysis (TGA)
  - Measures the change in mass of a sample as it is heated or cooled.
  - Applications: Decomposition temperatures, moisture content, filler content, and thermal stability.
3. Dynamic Mechanical Analysis (DMA)
  - Applies oscillatory stress to a material and measures its mechanical properties (e.g., stiffness and damping) as a function of temperature.
  - Applications: Viscoelastic behavior, glass transition temperature ( $T_g$ ), and polymer relaxation.
4. Thermomechanical Analysis (TMA)

---

- Measures dimensional changes (expansion, contraction) of a material under a controlled temperature program.

- Applications: Coefficient of thermal expansion (CTE), softening points.

#### 5. Differential Thermal Analysis (DTA)

- Measures temperature differences between a sample and a reference material as they are heated or cooled.

- Applications: Phase transitions, reactions, and thermal events.

#### 6. Evolved Gas Analysis (EGA)

- Analyzes gases released during heating (often coupled with TGA-MS or TGA-FTIR).

- Applications: Decomposition pathways, volatile content.

#### **I.4.3.2.Applications of Thermal Analysis:**

- Polymers: Glass transition ( $T_g$ ), melting, curing, oxidative stability.
- Pharmaceuticals: Polymorphism, purity, drug stability.
- Metals & Alloys: Phase transformations, recrystallization.
- Ceramics & Composites: Sintering behavior, thermal degradation.
- Food Science: Water content, fat crystallization.

#### **I.4.3.3.Key Parameters Measured:**

- Melting Point ( $T_m$ ) – DSC, DTA
- Glass Transition Temperature ( $T_g$ ) – DSC, DMA
- Decomposition Temperature – TGA
- Coefficient of Thermal Expansion (CTE) – TMA
- Heat Capacity ( $C_p$ ) – DSC

#### **I.4.3.4.Advantages of Thermal Analysis:**

- Fast & Precise: Small sample sizes, rapid results.
- Versatile: Applicable to solids, liquids, and powders.
- Quantitative & Qualitative: Provides both numerical data and insights into material behavior

In summary, organic waste represents a significant portion of global waste streams, varying widely in composition based on source and context. Recognizing the physical, chemical, and biological characteristics of these materials is crucial for optimizing treatment processes and minimizing environmental impact. With proper management, organic waste can be transformed from a burden into a valuable resource, contributing to soil health, renewable energy production, and circular economy goals.

# **Chapter II**

# **Gasification of**

# **Organic Waste**

## II.1.State of the Art in Gasification of Organic Waste

As the global community seeks cleaner and more sustainable energy alternatives, the conversion of organic waste into useful energy has gained growing attention. Gasification presents a promising thermochemical method for transforming biomass and other organic materials into syngas—a versatile energy carrier composed mainly of hydrogen and carbon monoxide. This chapter explores the principles of gasification, the underlying chemical reactions, and the influence of key process variables. It also examines how gasification compares to other waste-to-energy techniques, highlighting its potential for efficient energy recovery with reduced environmental impact.

### II.1.1.Principles of gasification

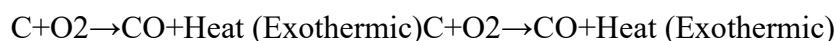
Gasification is a thermochemical process that converts carbonaceous materials (such as coal, biomass, or waste) into a mixture of gases known as syngas (synthesis gas), primarily composed of carbon monoxide (CO), hydrogen (H<sub>2</sub>), methane (CH<sub>4</sub>), and carbon dioxide (CO<sub>2</sub>). This process occurs in a controlled environment with limited oxygen (partial oxidation) or steam.

#### II.1.1.1Key Principles of Gasification

##### 1. Partial Oxidation

- Gasification occurs in an oxygen-deficient environment (typically 20-40% of the stoichiometric oxygen required for complete combustion).

- The chemical reaction can be represented as:



##### 2. Thermal Decomposition (Pyrolysis)

- At high temperatures (700–1,200°C), the feedstock undergoes pyrolysis, breaking down into volatile gases, liquids (tars), and solid char.

- Pyrolysis reactions release hydrocarbons, water vapor, and other volatile compounds.

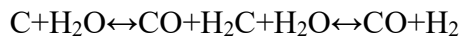
##### 3. Char Gasification Reactions

- The remaining solid char reacts with gases (CO<sub>2</sub>, H<sub>2</sub>O, H<sub>2</sub>) to produce syngas:

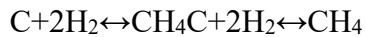
- Boudouard Reaction:



- Water-Gas Reaction:



- Methanation Reaction:



#### 4. Syngas Formation & Upgrading

○ The resulting gas mixture (CO, H<sub>2</sub>, CH<sub>4</sub>, CO<sub>2</sub>, and traces of other gases) can be further processed (e.g., water-gas shift reaction) to adjust the H<sub>2</sub>/CO ratio for different applications (fuel, chemicals, power generation).

#### 5. Heat Management

○ Gasification can be autothermal (self-sustaining via exothermic reactions) or allothermal (external heat source required, e.g., plasma gasification).

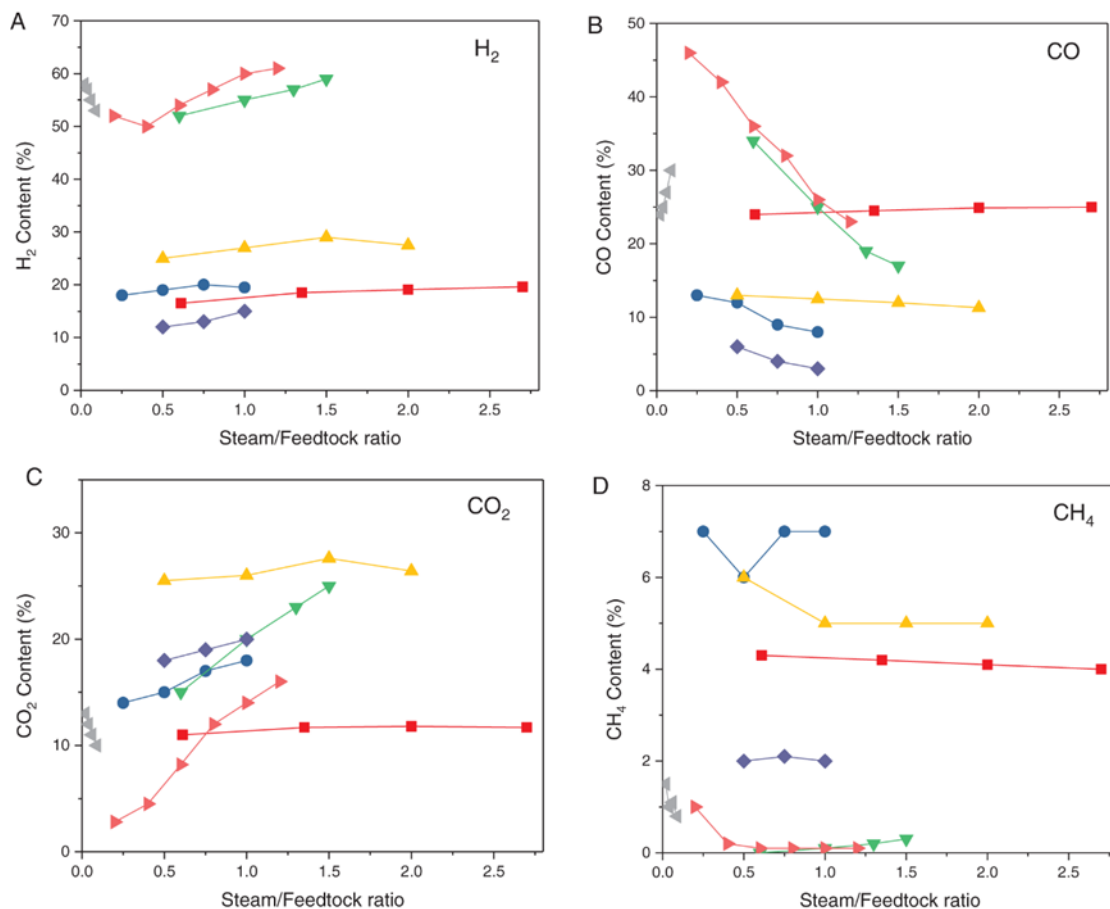
### II.1.1.2. Types of Gasifiers

- Fixed-Bed (Moving-Bed) Gasifiers (Updraft, Downdraft)
- Fluidized-Bed Gasifiers (Bubbling, Circulating)
- Entrained-Flow Gasifiers (High-temperature, ash slagging)
- Plasma Gasifiers (Ultra-high temperature, waste treatment)

### II.1.1.3. Applications of Gasification

- Power Generation (IGCC - Integrated Gasification Combined Cycle)
- Hydrogen & Synthetic Fuels Production (Fischer-Tropsch process)
- Chemical Feedstock (Methanol, ammonia, etc.)
- Waste-to-Energy (Municipal solid waste, hazardous waste treatment)

### II.1.1.4. Advantages



**Figure 2:** Influence of the steam/biomass ratio on the gas composition for the air and steam gasification of biowaste feedstock

- Converts low-value feedstocks (biomass, waste) into high-value energy.
- Lower emissions compared to direct combustion.
- Flexible in fuel input (coal, biomass, plastics).

### II.1.1.5. Challenges

- Tar formation (requires cleanup).
- High capital and operational costs.
- Complex process control.

### II.1.2. Gasification technologies

Gasification is a thermochemical process that converts carbonaceous materials (such as coal, biomass, waste, or petcoke) into syngas (primarily CO, H<sub>2</sub>, CO<sub>2</sub>, CH<sub>4</sub>, and small amounts of

other gases) by reacting the feedstock at high temperatures (typically **700–1,500°C**) with a controlled amount of oxygen and/or steam. This syngas can be used for power generation, chemical production, or fuel synthesis.

### **II.1.2.1.Key Gasification Technologies**

Gasification technologies vary based on reactor design, feedstock, and application. The main types include:

#### **II.1.2.1.a. Fixed (Moving) Bed Gasifiers**

- Description: Feedstock moves downward while gasifying agents (air, oxygen, or steam) flow upward.

- Types:

- Updraft (Counter-current): Syngas exits at the top, tar-rich.
- Downdraft (Co-current): Syngas exits at the bottom, lower tar content.

- Advantages: Simple design, good for small-scale applications.

- Disadvantages: Limited scalability, high tar production (updraft).

- Examples: Lurgi dry ash gasifier (historically used for coal).

#### **II.1.2.1.b.Fluidized Bed Gasifiers**

- Description: Feedstock is suspended in a bed of inert material (e.g., sand) by upward-flowing gas.

- Types:

- Bubbling Fluidized Bed (BFB): Lower gas velocity, good for high-ash feedstocks.
- Circulating Fluidized Bed (CFB): Higher gas velocity, better mixing, and efficiency.

- Advantages: Flexible feedstock (biomass, waste), uniform temperature.

- Disadvantages: Lower syngas quality (higher particulates), moderate tar levels.

- Examples: Foster Wheeler, KBR gasifiers.

#### **II.1.2.1.c.Entrained Flow Gasifiers**

- Description: Feedstock is finely ground and injected with oxygen/steam at high velocity (slagging conditions).

- Advantages: High efficiency, very low tar, suitable for coal and petcoke.

- Disadvantages: High operating temperature, expensive oxygen requirement.

- Examples:

- Shell Gasifier (coal, waste)

- GE (Texaco) Gasifier (slurry feed)

- Siemens (FutureEnergy) Gasifier

#### II.1.2.1.d. Plasma Gasifiers

- Description: Uses plasma torches (5,000–15,000°C) to break down feedstock into syngas and vitrified slag.

- Advantages: Can process hazardous waste, very clean syngas.

- Disadvantages: High energy consumption, expensive.

- Examples: Westinghouse Plasma, Alter NRG.

#### II.1.2.2. Applications of Gasification

- Power Generation (IGCC – Integrated Gasification Combined Cycle)

- Chemical Production (methanol, ammonia, Fischer-Tropsch fuels)

- Hydrogen Production (for refining or fuel cells)

- Waste-to-Energy (MSW, hazardous waste treatment)

**Table 3:** Comparison of Gasification Technologies

Parameter	Fixed Bed	Fluidized Bed	Entrained Flow	Plasma
Temperature	700–1,000°C	800–1,000°C	1,200–1,500°C	>5,000°C
Feedstock Size	Large chunks	Small particles	Fine powder	Any form
Tar Production	High (updraft)	Moderate	Very Low	None

Parameter	Fixed Bed	Fluidized Bed	Entrained Flow	Plasma
Oxygen Need	Low	Moderate	High	Very High
Scalability	Small-Medium	Medium-Large	Large	Small-Medium

### II.1.2.3. Emerging Trends

- Biomass & Waste Gasification: For renewable energy and circular economy.
- Hydrogen from Gasification: With carbon capture (blue hydrogen).
- Hybrid Systems: Combining gasification with pyrolysis or anaerobic digestion.

### II.1.3. Characteristics of the produced syngas

Syngas, or synthesis gas, is a mixture primarily composed of hydrogen ( $H_2$ ) and carbon monoxide (CO), along with smaller amounts of carbon dioxide ( $CO_2$ ), methane ( $CH_4$ ), water vapor ( $H_2O$ ), and sometimes nitrogen ( $N_2$ ) or other trace gases. Its characteristics depend on the feedstock and production method (e.g., steam reforming, gasification, or partial oxidation). Here are the key characteristics of syngas:

#### II.1.3.1. Composition

- Primary Components:
  - $H_2$  (Hydrogen) – 20–40% (varies with process)
  - CO (Carbon Monoxide) – 30–60%
- Secondary Components:
  - $CO_2$  (Carbon Dioxide) – 5–15%
  - $CH_4$  (Methane) – 0–10%
  - $N_2$  (Nitrogen) – Present if air is used in gasification
  - $H_2O$  (Water Vapor) – Depends on cooling and cleaning
  - Trace impurities (e.g.,  $H_2S$ ,  $NH_3$ , tars, particulates) – Require removal for downstream use.

#### II.1.3.2. Heating Value

- Lower Heating Value (LHV): Typically 10–20 MJ/Nm<sup>3</sup> (varies with H<sub>2</sub>/CO ratio).
  - Higher if methane is present.
  - Lower if diluted with CO<sub>2</sub> or N<sub>2</sub>.

### **II.1.3.3.H<sub>2</sub>/CO Ratio**

- Ranges from 0.5 to 3, depending on the process:
  - Coal gasification: ~0.5–1 (low H<sub>2</sub>/CO).
  - Steam methane reforming (SMR): ~3–5 (high H<sub>2</sub>/CO).
  - Adjustable via the water-gas shift (WGS) reaction ( $\text{CO} + \text{H}_2\text{O} \rightarrow \text{CO}_2 + \text{H}_2$ ).

### **II.1.3.4.Purity & Contaminants**

- May contain sulfur compounds (H<sub>2</sub>S, COS), particulates, tars, and alkali metals (from biomass/coal).
- Requires cleaning (scrubbers, filters, catalytic reactors) for most applications.

### **II.1.3.5.Applications**

- Fuel: Can be combusted for heat/power (after cleaning).
- Chemical Synthesis: Feedstock for:
  - Fischer-Tropsch fuels (liquid hydrocarbons).
  - Methanol/DME production.
  - Ammonia (NH<sub>3</sub>) synthesis (if H<sub>2</sub>-rich).
  - Hydrogen production (via CO removal).

### II.1.3.6. Production Methods & Their Influence

**Table 4:** Production Methods & Their Influence

Method	Typical H <sub>2</sub> /CO Ratio	Key Features
Steam Reforming (SMR)	3–5	High H <sub>2</sub> , low CO; uses natural gas.
Partial Oxidation (POX)	~1.8–2.2	Balanced H <sub>2</sub> /CO; uses O <sub>2</sub> .
Coal/Biomass Gasification	0.5–1.5	Low H <sub>2</sub> , high CO; produces tars/ash.
Autothermal Reforming (ATR)	~2.5	Combines SMR & POX.

### II.1.3.7. Challenges

- Tar formation (in biomass gasification).
- High CO<sub>2</sub> emissions (unless captured via CCS).
- Energy-intensive purification (for sensitive catalysts in synthesis).

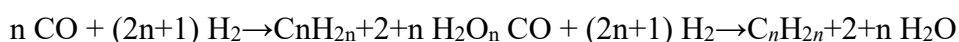
### II.1.4. Valorization of syngas

The valorization of syngas (synthesis gas, a mixture of CO, H<sub>2</sub>, and CO<sub>2</sub>) involves converting it into valuable chemicals, fuels, and energy. Syngas can be produced from various feedstocks, including biomass, coal, natural gas, and waste, via gasification or reforming processes. Below are the key pathways for syngas valorization:

#### II.1.4.1. Fuel Production

- Fischer-Tropsch Synthesis (FTS):

Converts syngas into liquid hydrocarbons (diesel, jet fuel, waxes) using Fe- or Co-based catalysts.



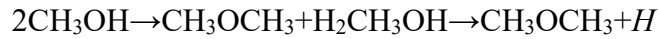
- Methanol Synthesis:

Syngas is converted to methanol over Cu/ZnO/Al<sub>2</sub>O<sub>3</sub> catalysts, which can be further processed into fuels (MTBE, DME) or chemicals.



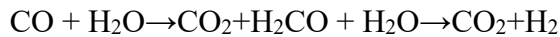
- DME (Dimethyl Ether) Production:

Methanol is dehydrated to DME, a clean-burning fuel and LPG substitute.



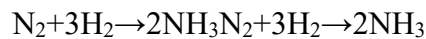
- Hydrogen Production (for fuel cells or ammonia synthesis):

Syngas undergoes the Water-Gas Shift (WGS) reaction to maximize H<sub>2</sub> yield.



#### II.1.4.2. Chemical Synthesis

- Ammonia (NH<sub>3</sub>) Production (Haber-Bosch process):



- Oxo-Synthesis (Hydroformylation):

Produces aldehydes/alcohols from olefins (e.g., propylene → butyraldehyde).



- Acetic Acid & Derivatives:

Methanol carbonylation yields acetic acid.



#### II.1.4.3. Power Generation

- Combined Heat and Power (CHP):

Syngas can be burned in gas turbines/engines for electricity and heat.

- Integrated Gasification Combined Cycle (IGCC):

High-efficiency power generation with CO<sub>2</sub> capture potential.

#### II.1.4.4. Waste-to-Energy & Carbon Capture

- Plastic & Waste Gasification:

Converts non-recyclable waste into syngas for energy/chemicals.

- CO<sub>2</sub> Utilization:

Syngas with high CO<sub>2</sub> can be used in methanation (Power-to-Gas) or electrofuels production.



### Challenges & Innovations

- Catalyst Development: Improving selectivity for desired products (e.g., lower methane formation in FTS).
- H<sub>2</sub>/CO Ratio Adjustment: Using WGS or CO<sub>2</sub> hydrogenation to optimize feedstocks.
- Sustainability: Coupling with biomass gasification or green H<sub>2</sub> for carbon-neutral processes.

### II.1.5. Factors influencing the gasification of organic waste

The gasification of organic waste is a thermochemical process that converts carbonaceous materials into syngas (primarily CO, H<sub>2</sub>, CO<sub>2</sub>, and CH<sub>4</sub>) under controlled conditions. Several factors influence the efficiency, yield, and composition of the produced syngas. Below are the key factors along with references to relevant studies:

#### II.1.5.1. Feedstock Characteristics

- Moisture Content: High moisture content reduces thermal efficiency and increases energy consumption for evaporation [1].
- Particle Size & Density: Smaller particles enhance heat and mass transfer but may cause fluidization issues [2].
- Ash Content: High ash content can lead to slagging and fouling, reducing gasifier efficiency [3].
- Volatile Matter & Fixed Carbon: Higher volatile matter increases gas yield, while fixed carbon affects char formation [4].

#### II.1.5.2. Gasification Temperature

- Higher temperatures (>700°C) favor endothermic reactions, increasing H<sub>2</sub> and CO production while reducing tar formation [5].

- Excessive temperatures may increase energy costs and ash melting [6].

#### **II.1.5.3. Equivalence Ratio (ER)**

• The ratio of actual air supplied to stoichiometric air requirement affects combustion efficiency. Optimal ER (0.2–0.4) balances oxidation and gasification [7].

#### **II.1.5.4. Gasifying Agent**

- Air: Produces low-calorific syngas (4–7 MJ/Nm<sup>3</sup>) due to N<sub>2</sub> dilution [8].
- Oxygen/Steam: Enhances H<sub>2</sub> production via water-gas shift reaction [9].
- CO<sub>2</sub>: Can be used for dry reforming, increasing CO yield [10].

#### **II.1.5.5. Residence Time**

- Longer residence time improves conversion efficiency but may reduce throughput [11].

#### **II.1.5.6. Catalyst Use**

• Catalysts (e.g., Ni, dolomite, olivine) reduce tar formation and enhance H<sub>2</sub> yield (Sutton et al., 2001)[12].

#### **II.1.5.7. Pressure**

- Pressurized gasification improves energy density but requires robust reactor designs[13].

#### **II.1.5.8. Reactor Type**

- Fixed-bed: Suitable for small-scale applications but has limited scalability [11].
- Fluidized-bed: Better mixing and higher efficiency but more complex operation [6].
- Entrained-flow: High-temperature operation for clean syngas but high [8].

### **II.2. Analysis of Existing Processes for the Valorization of Organic Waste**

#### **II.2.1. Incineration**

Incineration is a waste treatment process that involves the combustion of organic substances contained in waste materials. It converts waste into ash, flue gas, and heat, which can sometimes be used to generate electricity. Here's a detailed breakdown:

##### **II.2.1.1. How Incineration Works**

1. Waste Delivery & Preparation – Waste is collected, sorted (to remove non-combustibles like metals), and fed into the incinerator.

2. Combustion Chamber – Waste is burned at high temperatures (typically 850–1,200°C), reducing it to ash and gas.

3. Energy Recovery (Optional) – Heat from combustion can boil water, producing steam to drive turbines for electricity (Waste-to-Energy, WtE).

4. Pollution Control – Flue gases pass through scrubbers, filters (e.g., activated carbon, baghouses), and electrostatic precipitators to remove pollutants like:

- Particulate matter (dust)
- Acid gases (HCl, SO<sub>2</sub>)
- Toxic compounds (dioxins, furans, heavy metals)

5. Ash Disposal – Residual ash (10–20% of original waste volume) is landfilled or reused (e.g., in construction if non-toxic).

### **II.2.1.2. Advantages of Incineration**

Volume Reduction – Reduces waste volume by ~90%, extending landfill lifespans.

Energy Recovery – Can generate electricity or heat for district heating.

Pathogen Destruction – High temperatures eliminate hazardous biological waste.

Controlled Emissions – Modern plants have strict pollution controls (unlike open burning).

### **II.2.1.3. Disadvantages & Concerns**

Air Pollution – Even with controls, some emissions (CO<sub>2</sub>, NO<sub>x</sub>, dioxins) persist.

Toxic Ash – Fly ash may contain heavy metals (Pb, Cd, Hg), requiring special disposal.

High Costs – Expensive to build and maintain (especially with emission controls).

Public Opposition – NIMBY ("Not In My Backyard") concerns over health risks.

CO<sub>2</sub> Emissions – Burning plastics and organic waste contributes to greenhouse gases.

### **II.2.1.4. Alternatives to Incineration**

- Recycling & Composting – Better for reducing waste at the source.
- Anaerobic Digestion – Breaks down organic waste without combustion.
- Landfill Gas Capture – Extracts methane from decomposing waste for energy.

**II.2.2.Composting:**

Composting is the natural process of recycling organic matter, such as food scraps and yard waste, into a nutrient-rich soil amendment called compost. This process is facilitated by microorganisms (bacteria, fungi), insects, and worms that break down organic materials under controlled conditions.

**II.2.2.1.Benefits of Composting:**

1. Reduces Waste – Diverts organic materials from landfills, reducing methane emissions.
2. Enriches Soil – Improves soil structure, moisture retention, and fertility.
3. Reduces Need for Chemical Fertilizers – Compost provides essential nutrients naturally.
4. Supports Plant Growth – Helps plants resist diseases and pests.
5. Lowers Carbon Footprint – Decreases greenhouse gas emissions from waste decomposition in landfills.

**II.2.2.2.What Can Be Composted?****II.2.2.2.a.Greens (Nitrogen-rich materials):**

- Fruit & vegetable scraps
- Coffee grounds & filters
- Tea bags (non-plastic)
- Fresh grass clippings
- Plant trimmings

**II.2.2.2.b.Browns (Carbon-rich materials):**

- Dry leaves
- Straw & hay
- Cardboard (shredded, uncoated)
- Newspaper (black & white, shredded)
- Wood chips & sawdust (untreated)

**II.2.2.2.c.What NOT to Compost:**

- Meat, fish, or dairy (can attract pests)
- Oily or greasy foods
- Pet waste (may contain pathogens)
- Diseased plants
- Glossy or coated paper
- Synthetic materials (plastic, metal)

### **II.2.2.3.How to Start Composting:**

#### **II.2.2.3.a.Choose a Method:**

- Backyard Composting: Use a bin or pile in your yard.
- Indoor Composting (Vermicomposting): Use worms in a small bin.
- Bokashi: Ferment food waste in an airtight container.

#### **II.2.2.3.b.Layer Greens & Browns:**

- Alternate wet (greens) and dry (browns) materials for balance.
- Ideal ratio: 3 parts browns to 1 part greens.

#### **II.2.2.3.c.Maintain the Compost:**

- Aerate: Turn the pile regularly for oxygen.
- Moisture: Keep it damp (like a wrung-out sponge).
- Size: A 3x3 ft pile helps retain heat for faster breakdown.

#### **II.2.2.3.d.Wait & Harvest:**

- Compost is ready in 2 months to 2 years, depending on conditions.
- Finished compost is dark, crumbly, and earthy-smelling.

### **II.2.2.4.Common Problems & Solutions:**

- Smelly Compost? → Add more browns and aerate.
- Not Breaking Down? → Check moisture, balance greens/browns, and chop materials smaller.

- Attracting Pests? → Avoid meat/dairy, bury food scraps, and use a closed bin.

#### **II.2.2.5. Uses for Finished Compost:**

- Mix into garden soil
- Use as mulch
- Make compost tea (liquid fertilizer)
- Top-dress lawns

### **II.2.3. Anaerobic Digestion**

#### **II.2.3.1. Definition**

Anaerobic digestion (AD) is a biological process in which microorganisms break down biodegradable organic matter in the absence of oxygen, producing biogas (a mixture of methane, CO<sub>2</sub>, and trace gases) and digestate (a nutrient-rich byproduct).

#### **II.2.3.2. Key Stages of Anaerobic Digestion**

The AD process occurs in four main stages:

1. Hydrolysis – Complex organic polymers (carbohydrates, proteins, fats) are broken down into simpler monomers (sugars, amino acids, fatty acids) by hydrolytic bacteria[26].
2. Acidogenesis – Acidogenic bacteria convert monomers into volatile fatty acids (VFAs), alcohols, hydrogen, and CO<sub>2</sub>.
3. Acetogenesis – Acetogenic bacteria further break down VFAs into acetic acid, hydrogen, and CO<sub>2</sub>[27].
4. Methanogenesis – Methanogenic archaea convert acetic acid, hydrogen, and CO<sub>2</sub> into methane (CH<sub>4</sub>) and CO<sub>2</sub>.

#### **II.2.3.3. Types of Anaerobic Digestion Systems**

- Wet AD (low solids, <15% TS) – Suitable for slurry and wastewater.
- Dry AD (high solids, >15% TS) – Used for solid waste like crop residues.
- Mesophilic (30–40°C) – Common for municipal waste.
- Thermophilic (50–60°C) – Faster but less stable.

#### **II.2.3.4.Applications & Benefits**

- Biogas Production: Used for electricity, heat, or vehicle fuel (upgraded to biomethane).
- Waste Management: Reduces landfill use and greenhouse gas emissions.
- Digestate Use: Acts as a biofertilizer, improving soil health.
- Carbon Neutrality: Helps in circular economy models.

#### **II.2.3.5.Challenges**

- Process instability due to pH fluctuations or ammonia inhibition.
- High capital and operational costs for large-scale plants.
- Contaminants in feedstock (plastics, heavy metals) can hinder efficiency[28].

#### **II.2.4.Pyrolysis:**

Pyrolysis is a thermochemical decomposition process that occurs in the absence of oxygen, converting organic materials into solid (char), liquid (bio-oil), and gaseous (syngas) products. It is widely used in waste management, biofuel production, and chemical manufacturing.

##### **II.2.4.1.Pyrolysis Process and Types**

Pyrolysis involves heating biomass or waste materials (typically between 300°C and 900°C) in an oxygen-free environment. The process can be categorized into:

- Slow Pyrolysis: Low heating rates (5–30°C/min), longer residence time, maximizes char production[15].
- Fast Pyrolysis: High heating rates (100–1000°C/s), short residence time (~2 sec), maximizes bio-oil yield.
- Flash Pyrolysis: Extremely rapid heating, very short residence time, maximizes liquid and gas products[16].

##### **II.2.4.2.Applications of Pyrolysis**

- Biofuel Production: Bio-oil can be upgraded into transportation fuels[17].
- Waste Management: Plastic and tire pyrolysis reduces landfill waste.
- Carbon Materials: Biochar is used for soil amendment and carbon sequestration.

- Syngas Production: Used for heat and electricity generation[18].

#### **II.2.4.3.Challenges and Future Perspectives**

- Economic Viability: High energy input costs.
- Product Quality: Bio-oil requires upgrading for commercial use[19].
- Scalability: Industrial-scale pyrolysis plants need optimization.

#### **II.3.Comparison of Different Valorization Techniques and Selection of Gasification**

Valorization techniques convert waste or low-value materials into useful products, such as energy, chemicals, or fuels. Below is a comparison of key valorization methods, followed by a justification for selecting gasification.

### II.3.1. Comparison of Valorization Techniques

**Table 5:** Comparison of Valorization Techniques

Technique	Process Description	Advantages	Disadvantages	References
Incineration	Direct combustion of waste at high temperatures to produce heat and electricity.	<ul style="list-style-type: none"> <li>- High energy recovery</li> <li>- Volume reduction of waste</li> </ul>	<ul style="list-style-type: none"> <li>- Air pollution (NO<sub>x</sub>, SO<sub>x</sub>, dioxins)</li> <li>- High CO<sub>2</sub> emissions</li> </ul>	[1], [2]
Pyrolysis	Thermal decomposition in the absence of oxygen to produce bio-oil, syngas, and char.	<ul style="list-style-type: none"> <li>- Produces liquid fuels (bio-oil)</li> <li>- Lower emissions than incineration</li> </ul>	<ul style="list-style-type: none"> <li>- Requires feedstock pretreatment</li> <li>- High operational costs</li> </ul>	[3], [4]
Anaerobic Digestion	Biological breakdown of organic waste to produce biogas (methane + CO <sub>2</sub> ).	<ul style="list-style-type: none"> <li>- Renewable energy (biogas)</li> <li>- Low emissions</li> </ul>	<ul style="list-style-type: none"> <li>- Slow process</li> <li>- Limited to organic waste</li> </ul>	[5], [23]
Gasification	Partial oxidation at high temperatures to produce syngas (CO + H <sub>2</sub> ).	<ul style="list-style-type: none"> <li>- Flexible feedstock (biomass, plastics, MSW)</li> <li>- Cleaner than incineration</li> </ul>	<ul style="list-style-type: none"> <li>- High capital cost</li> <li>- Tar formation issues</li> </ul>	[4], [24]
Landfilling	Waste disposal in landfills with possible methane capture.	<ul style="list-style-type: none"> <li>- Low initial cost</li> </ul>	<ul style="list-style-type: none"> <li>- Methane leakage (GHG emissions)</li> <li>- Land use issues</li> </ul>	[9]

### II.3.2. Selection of Gasification

Gasification is often preferred over other valorization techniques due to:

### II.3.3. Advantages of Gasification:

Higher Energy Efficiency: Produces syngas ( $\text{CO} + \text{H}_2$ ), which can be used for electricity, hydrogen, or synthetic fuels.

Waste Flexibility: Can process diverse feedstocks (biomass, municipal solid waste, plastics).

Lower Emissions: Compared to incineration, it generates fewer pollutants (e.g., dioxins,  $\text{SO}_x$ ).

Carbon Capture Potential: Syngas can be utilized in carbon-neutral or carbon-negative processes.

### II.3.4. Challenges & Mitigation:

- Tar Formation: Can clog systems, but advanced gasifiers (plasma, fluidized bed) minimize this issue [24].

- High Capital Cost: Offset by long-term sustainability benefits and government incentives [26].

### II.3.5. Case Studies & Applications:

- Waste-to-Energy (WtE): Gasification of MSW reduces landfill dependency [4].

- Biomass Conversion: Produces renewable hydrogen and biofuels [25].

### II.3.6. Conclusion

While each valorization method has merits, gasification stands out due to its feedstock flexibility, cleaner syngas output, and potential for circular economy integration. It is particularly suitable for sustainable waste management and energy recovery.

Gasification has emerged as a viable pathway for converting organic waste into energy-rich syngas, offering a flexible and relatively clean alternative to conventional waste treatment methods. While technical and economic challenges remain, especially regarding tar removal and system efficiency, advancements in gasifier design and feedstock preparation are steadily improving outcomes. Ultimately, integrating gasification into waste management systems can contribute significantly to reducing landfill dependence and promoting a circular energy economy.

# **Chapter III: The Gasifier**

At the heart of the gasification process lies the gasifier—a specialized reactor where thermal decomposition of organic material occurs under controlled conditions. The design, configuration, and operating parameters of gasifiers play a critical role in determining the quality and efficiency of syngas production. This chapter provides an in-depth look at the various types of gasifiers, including fixed-bed, fluidized-bed, and plasma-based systems. It further analyzes the advantages and limitations of each type, offering insight into their suitability for different scales and types of organic waste.

### **III.1. Choice of Gasifier and Operating Conditions**

#### **III.1.1.Type of gasifier (fixed bed, fluidized bed, plasma, etc.)**

Gasifiers are classified based on their design and the method of contacting fuel with the gasifying agent (air, oxygen, steam). Below are the main types of gasifiers with references:

##### **III.1.1.1 Fixed Bed (Moving Bed) Gasifiers**

###### **III.1.1.1.a. Updraft (Counter-current) Gasifier:**

- Fuel moves downward, while the gasifying agent flows upward.
- Produces tar-rich gas, suitable for dry fuels[13].

###### **III.1.1.1.b. Downdraft (Co-current) Gasifier:**

- Fuel and gasifying agent move downward.
- Lower tar content, suitable for small-scale applications[14].

###### **III.1.1.1.c.Cross-draft Gasifier:**

- Air enters from the side, producing high-temperature gas.
- Used for high-ash fuels[8].

##### **III.1.1.2.Fluidized Bed Gasifiers**

###### **III.1.1.2.a.Bubbling Fluidized Bed (BFB):**

- Fuel is suspended in a bed of inert material (e.g., sand)[11].
- Good heat transfer, handles high-ash fuels.

**III.1.1.2.b.Circulating Fluidized Bed (CFB):**

- Higher gas velocity recirculates bed material.
- Suitable for large-scale applications[33].

**III.1.1.2.c.Dual Fluidized Bed (DFB):**

- Separates combustion and gasification zones.
- Produces high-quality syngas (low nitrogen dilution)[34].

**III.1.1.3. Entrained Flow Gasifiers**

- Operate at high temperatures ( $>1200^{\circ}\text{C}$ ) and pressures.
- Suitable for coal and liquid feedstocks[35].

**III.1.1.4.Plasma Gasifiers**

- Use plasma torches ( $>2000^{\circ}\text{C}$ ) to decompose waste into syngas and slag.
- Handles hazardous and non-biodegradable waste[36].

**III.1.1.5.Supercritical Water Gasification (SCWG)**

- Gasification in water above its critical point ( $374^{\circ}\text{C}$ , 22.1 MPa).
- Suitable for wet biomass[37].

**III.1.2.Gasification temperature**

The gasification temperature typically ranges between  $500^{\circ}\text{C}$  and  $1,500^{\circ}\text{C}$ , depending on the feedstock, gasifying agent, and type of gasifier used. Below is a breakdown of gasification temperatures for different processes, along with references:

**III.1.2.1. General Gasification Temperature Ranges****III.1.2.1.a.Low-temperature gasification:  $500\text{--}800^{\circ}\text{C}$** 

- Used for biomass and waste gasification.
- Produces more tars and methane.

**III.1.2.1.b. Medium-temperature gasification:  $800\text{--}1,200^{\circ}\text{C}$** 

- Common for air-blown and steam gasification.

- Reduces tar formation.

Endothermic	Exothermic
<p><b>Hydrocarbons reforming:</b></p> $C_nH_m + 2nH_2O \rightarrow (2n+m/2)H_2 + nCO_2$	<p><b>Shift / Water-Gas Shift Reaction</b> (300-600 °C)</p> $CO + H_2O \leftrightarrow CO_2 + H_2$
<p><b>Methane Decomposition</b> (&gt; 500 °C)</p> $CH_4 + H_2O \leftrightarrow CO + 3H_2$ $CH_4 + 2H_2O \leftrightarrow CO_2 + H_2$	<p><b>Steam Reforming Reaction</b> (&gt; 700 °C)</p> $C_nH_m + 2nH_2O \leftrightarrow (2n+m/2)H_2 + nCO_2$
<p><b>Boudouard Reaction</b> (&gt; 700 °C)</p> $C + CO_2 \leftrightarrow 2CO$	<p><b>Methane Forming reaction</b> (300-600 °C)</p> $CO + 3H_2 \leftrightarrow CH_4 + H_2O$ $CO_2 + H_2 \leftrightarrow CH_4 + 2H_2O$
<p><b>Water-Gas (Primary) Reaction</b> (&gt; 700 °C)</p> $C + H_2O \leftrightarrow CO + H_2$ $C + 2H_2O \leftrightarrow CO_2 + 2H_2$	<p><b>Combustion of Char</b></p> $C + O_2 \leftrightarrow CO_2$
<p><b>Secondary Tar Cracking</b></p> $Tar + H_2O \rightarrow H_2 + CO$ $Tar + H_2 \rightarrow \text{light hydrocarbons} + \text{gases}$ $Tar + xH_2O \rightarrow yCO_2 + zH_2$ $Tar \rightarrow CH_4 + H_2 + H_2O + C_nH_m$	<p style="text-align: center;"><b>Steam gasification reaction</b></p> $C_xH_yO_z + \text{heat} \rightarrow \text{steam} + \text{gas} + \text{tar}$

**Figure 3:** Typical gasification mechanism from organic waste during steam gasification

### III.1.2.1.c. High-temperature gasification: 1,200–1,500°C

- Used in oxygen-blown and plasma gasification.
- Maximizes syngas ( $H_2 + CO$ ) yield with minimal tar.

### III.1.2.2. Gasification Temperatures by Gasifier Type

**Table 6:** Gasification Temperatures by Gasifier Type

Gasifier Type	Temperature Range (°C)	References
Fixed-bed (Downdraft)	700–1,200	[38], [39]
Fixed-bed (Updraft)	500–1,000	[38], [40]
Fluidized Bed	800–1,000	[41], [42]
Entrained Flow	1,200–1,500	[43], [44]
Plasma Gasification	2,000–5,000 (localized)	[45], [46]

### III.1.3. Gasifying agent (air, steam, oxygen, etc.)

Gasifying agents are substances used to convert carbonaceous materials (like coal, biomass, or waste) into syngas (a mixture of H<sub>2</sub>, CO, CO<sub>2</sub>, CH<sub>4</sub>, and other gases) through gasification. The choice of gasifying agent significantly impacts the composition, heating value, and applications of the produced syngas. The most common gasifying agents are:

#### III.1.3.1. Air

##### III.1.3.1.a. Composition: ~21% O<sub>2</sub>, ~78% N<sub>2</sub>

##### III.1.3.1.b. Effects:

- Produces a low-calorific-value syngas (4–6 MJ/Nm<sup>3</sup>) due to nitrogen dilution.
- Lower reaction temperatures (~800–1000°C) compared to oxygen gasification.
- Cost-effective (no air separation unit required).

##### III.1.3.1.c. Applications:

- Small-scale biomass gasifiers, power generation[38][13].

#### III.1.3.2. Steam (H<sub>2</sub>O)

##### III.1.3.2.a. Effects:

- Enhances hydrogen (H<sub>2</sub>) production via the water-gas shift reaction:



- Produces medium-calorific-value syngas (10–15 MJ/Nm<sup>3</sup>).
- Requires external heat (endothermic reaction).

##### III.1.3.2.b. Applications:

- Hydrogen production, chemical synthesis (ammonia, methanol).[44][45]

#### III.1.3.3. Oxygen (O<sub>2</sub>)

##### III.1.3.3.a. Effects:

- Produces a nitrogen-free, medium-to-high calorific syngas (10–15 MJ/Nm<sup>3</sup>)[46].
- Higher temperatures (~1200–1500°C) enable better tar cracking.

- Requires an air separation unit (ASU), increasing costs.

#### III.1.3.3.b.Applications:

- Large-scale IGCC (Integrated Gasification Combined Cycle), Fischer-Tropsch synthesis[47].

#### III.1.3.4.Carbon Dioxide (CO<sub>2</sub>)

##### III.1.3.4.a.Effects:

- Acts as a weak oxidizer (Boudouard reaction):



- Can reduce greenhouse gas emissions when using captured CO<sub>2</sub>.

##### III.1.3.4.b.Applications:

- Experimental, CO<sub>2</sub> utilization strategies[48].

#### III.1.3.5.Air-Steam Mixtures

##### III.1.3.5.a.Effects:

- Balances exothermic oxidation (from air) with endothermic steam reactions.
- Improves H<sub>2</sub> yield compared to pure air gasification[49].

##### III.1.3.5.b.Applications:

- Dual-fluidized-bed gasifiers, medium-scale systems.

#### III.1.3.6.Comparison Table

**Table 7:** Comparison Table

Gasifying Agent	Syngas LHV (MJ/Nm <sup>3</sup> )	H <sub>2</sub> /CO Ratio	Key Advantages	Key Drawbacks
Air	4–6	Low (~0.5)	Low cost	Low H <sub>2</sub> , N <sub>2</sub> dilution
Steam	10–15	High (~2)	High H <sub>2</sub> yield	Energy-intensive

Gasifying Agent	Syngas LHV (MJ/Nm <sup>3</sup> )	H <sub>2</sub> /CO Ratio	Key Advantages	Key Drawbacks
Oxygen	10–15	Medium (~1)	No N <sub>2</sub> dilution	High ASU cost
CO <sub>2</sub>	8–12	Low (~0.7)	CO <sub>2</sub> utilization	Slow kinetics

### III.1.4. Gasification flow rate

The gasification flow rate refers to the rate at which a feedstock (such as coal, biomass, or waste) is converted into syngas (a mixture of CO, H<sub>2</sub>, CH<sub>4</sub>, and other gases) in a gasifier. The flow rate depends on factors like feedstock type, gasifier design, operating conditions (temperature, pressure), and desired syngas composition.

#### III.1.4.1. Typical Gasification Flow Rates

##### III.1.4.1.a. Coal Gasification

- Fixed-bed gasifiers: ~0.5–3 kg/(m<sup>2</sup>·s)
- Fluidized-bed gasifiers: ~0.1–1 m/s (superficial velocity)
- Entrained-flow gasifiers: ~2–10 kg/s (for large-scale systems)[50].

##### III.1.4.1.b. Biomass Gasification

- Downdraft gasifiers: ~1.5–3 kg/(m<sup>2</sup>·s)[51]
- Bubbling fluidized bed: ~0.5–2 m/s (gas velocity)
- Circulating fluidized bed: ~3–8 m/s (gas velocity)

##### III.1.4.1.c. Waste-to-Energy Gasification

- Plasma gasifiers: ~0.1–0.5 kg/s (for MSW processing)[52][53]

Reviews flow rates in waste gasification systems.

#### 1. DOE/NETL Reports (U.S. Department of Energy)

- Provide data on large-scale coal gasification flow rates (e.g., 2500–5000 tons/day plants).

### III.1.5. Ratio of gasifying agent to waste

The ratio of gasifying agent to waste is a critical parameter in gasification processes, as it affects the efficiency, syngas composition, and overall performance of the system. This ratio is typically expressed in terms of the mass or volume of gasifying agent (air, oxygen, steam, or CO<sub>2</sub>) per unit mass of waste feedstock[8][2].

#### III.1.5.1. Common Gasifying Agents and Their Ratios

##### III.1.5.1.a. Air Gasification

- Typical ratio: 1.5–3.5 Nm<sup>3</sup>/kg of waste (varies with waste type)
- Air is the most common gasifying agent due to its low cost, but it introduces nitrogen, diluting the syngas.
- Equivalence Ratio (ER): 0.2–0.4 (ratio of actual air to stoichiometric air required for combustion)

##### III.1.5.1.b. Oxygen Gasification

- Typical ratio: **0.3–0.8 kg O<sub>2</sub>/kg waste**
- Produces higher-quality syngas (higher H<sub>2</sub> and CO, less N<sub>2</sub> dilution).
- Requires an air separation unit (ASU), increasing costs.

##### III.1.5.1.c. Steam Gasification

- Typical ratio: 0.2–1.0 kg steam/kg waste
- Enhances hydrogen production via water-gas shift reaction.
- Often combined with oxygen or air to improve heat balance.

##### III.1.5.1.d. CO<sub>2</sub> Gasification

- Used less frequently but can help in carbon capture applications.[6]
- Typical ratio: 0.1–0.5 kg CO<sub>2</sub>/kg waste

#### III.1.5.2. Factors Influencing the Ratio

- Waste composition (moisture, ash, volatile matter)
- Gasifier type (fixed-bed, fluidized-bed, entrained-flow)

- Desired syngas composition (H<sub>2</sub>/CO ratio)[4]
- Temperature and pressure of gasification

### **III.2.Implementation of Gasification Experiments**

Implementation of Gasification Experiments: A Review

Introduction to Gasification Experimental Systems

Gasification experiments require carefully designed systems to convert carbonaceous materials into syngas (primarily CO, H<sub>2</sub>, CH<sub>4</sub>, and CO<sub>2</sub>) under controlled conditions. The implementation involves several key components and considerations:

#### **III.2.1. Experimental Setup Components**

Reactor Systems

- Fixed-bed reactors: Commonly used for small-scale experiments and fundamental studies (Lahijani et al., 2018)
- Fluidized-bed reactors: Provide better heat and mass transfer (Akkache et al., 2016)[54]
- Entrained-flow reactors: Suitable for high-temperature, short-residence-time studies (Zhang et al., 2019)[55]

Supporting Equipment

- Gas supply and control system (N<sub>2</sub>, O<sub>2</sub>, steam, air)
- Heating system (electric, microwave, or combustion-based)
- Temperature measurement and control
- Pressure regulation system
- Gas cleaning and conditioning units
- Gas analysis equipment (GC, MS, FTIR)

#### **III.2.2.Key Experimental Parameters**

Researchers typically investigate the effects of:

- Temperature: Usually 600-1400°C (higher temperatures favor gas production)

- Equivalence ratio (ER): Typically 0.2-0.4 for air gasification (Patra & Sheth, 2015)
- Steam-to-biomass ratio: For steam gasification (0.5-2.0 common range)[56]
- Residence time: Varies with reactor type (seconds to hours)
- Feedstock characteristics: Particle size, moisture content, composition

### **III.2.3. Measurement and Analysis Techniques**

#### Gas Analysis

- Gas chromatography (GC) for composition (Pinto et al., 2018)[57]
- Online mass spectrometry for real-time monitoring
- FTIR spectroscopy for specific gas components

#### Solid Residue Analysis

- Proximate and ultimate analysis
- SEM/EDS for morphology and elemental composition
- XRD for crystalline phase identification

#### Process Monitoring

- Temperature profiling (thermocouples, IR)
- Pressure monitoring
- Flow rate measurements

### **III.2.4. Safety Considerations**

Critical safety measures include:[58]

- Explosion-proof equipment design
- Gas leak detection systems
- Pressure relief devices
- Proper ventilation
- Emergency shutdown systems

### III.2.5. Data Processing and Analysis

Common approaches include:

- Mass and energy balance calculations
- Cold gas efficiency determination
- Carbon conversion efficiency
- Higher heating value (HHV) calculation of syngas
- Statistical analysis of experimental results.

## III.3. Analysis of Produced Syngas

### III.3.1 Analysis of Produced Syngas

Syngas (synthesis gas) is a crucial intermediate in chemical and energy industries, primarily composed of hydrogen (H<sub>2</sub>), carbon monoxide (CO), carbon dioxide (CO<sub>2</sub>), methane (CH<sub>4</sub>), and nitrogen (N<sub>2</sub>). Its composition varies depending on the feedstock and production method (e.g., steam reforming, gasification, or partial oxidation). Below is a detailed analysis of syngas composition, quality indicators, and applications, supported by references [59][.8]

#### III.3.1.1. Composition of Syngas

The composition of syngas depends on the production process and feedstock (coal, biomass, natural gas, waste):

**Table 8:** The composition of syngas depends on the production process and feedstock (coal, biomass, natural gas, waste)

Component	Typical Range (%)	Influence on Syngas Quality
H <sub>2</sub>	20–60%	Key for ammonia & fuel synthesis
CO	15–50%	Essential for Fischer-Tropsch & methanol synthesis
CO <sub>2</sub>	5–20%	Diluent; may require removal

Component	Typical Range (%)	Influence on Syngas Quality
CH <sub>4</sub>	0–15%	Can be reformed for more H <sub>2</sub> /CO
N <sub>2</sub>	0–5% (higher in air-blown gasification)	Inert, lowers heating value

### III.3.1.2. Key Quality Parameters

#### III.3.1.2.A. H<sub>2</sub>/CO Ratio

- Optimal for downstream processes:
  - Fischer-Tropsch synthesis: ~2.0
  - Methanol synthesis: ~2.0–2.1
  - Ammonia production: Requires pure H<sub>2</sub> (via water-gas shift reaction)

#### III.3.1.2.B. Heating Value

- Lower Heating Value (LHV):
  - 5–15 MJ/Nm<sup>3</sup> (for air-blown gasification)[60]
  - 10–20 MJ/Nm<sup>3</sup> (for oxygen-blown gasification)

#### III.3.1.2.C. Impurities (Tars, Particulates, Sulfur)

- Tars: Can clog systems; require catalytic cracking or scrubbing.[61]
- Sulfur (H<sub>2</sub>S, COS): Poisonous to catalysts; removed via amine scrubbing.

### III.3.1.3. Production Methods & Their Impact on Syngas Composition[62][63]

**Table9:** Production Methods & Their Impact on Syngas Composition

Method	H <sub>2</sub> /CO Ratio	Advantages	Disadvantages
Steam Reforming (SMR)	~3.0	High H <sub>2</sub> yield	High energy input

Method	H <sub>2</sub> /CO Ratio	Advantages	Disadvantages
Partial Oxidation (POX)	~1.7	No catalyst needed	Soot formation
Gasification (Biomass/Coal)	~0.5–1.5	Flexible feedstock	Tar & particulate issues
Auto-Thermal Reforming (ATR)	~2.0–2.5	Balanced H <sub>2</sub> /CO	Complex operation

#### III.3.1.4. Applications of Syngas

- Fischer-Tropsch Fuels: Conversion to liquid hydrocarbons (diesel, jet fuel).
- Methanol & DME Production: Key chemical feedstock.[64]
- Hydrogen Production: For ammonia synthesis or fuel cells.[65]
- Power Generation: Integrated Gasification Combined Cycle (IGCC).

#### III.3.1.5. Challenges & Future Trends

- Carbon Capture: Integration with CCS (Carbon Capture & Storage) for cleaner syngas.[66]
- Catalyst Development: Improved reforming/gasification catalysts for higher efficiency.
- Waste-to-Syngas: Plasma gasification for municipal waste conversion.[67]

#### III.3.1.6. Gas composition (CO, H<sub>2</sub>, CH<sub>4</sub>, CO<sub>2</sub>, N<sub>2</sub>, etc.)

The composition of gas mixtures, such as natural gas, syngas, biogas, and flue gas, varies depending on the source and production method. Below are typical compositions with references[68]:

### III.3.1.7. Natural Gas

Mainly consists of methane with minor amounts of other hydrocarbons and impurities:

- CH<sub>4</sub>: 70–90%
- C<sub>2</sub>H<sub>6</sub>: 0–20%
- C<sub>3</sub>H<sub>8</sub> & higher hydrocarbons: 0–10%
- CO<sub>2</sub>: 0–8%
- N<sub>2</sub>: 0–5%
- H<sub>2</sub>S: Trace amounts (varies by source)

### III.3.1.8. Syngas (Synthesis Gas)

Produced via gasification of coal, biomass, or steam reforming of methane:

- H<sub>2</sub>: 30–60%
- CO: 20–40%
- CO<sub>2</sub>: 5–15%
- CH<sub>4</sub>: 0–10%
- N<sub>2</sub>: 0–5% (depends on air or oxygen gasification)[69]

### III.3.1.3. Biogas (Anaerobic Digestion)

Produced from organic waste decomposition:

- CH<sub>4</sub>: 50–75%
- CO<sub>2</sub>: 25–50%
- H<sub>2</sub>: 0–3%
- N<sub>2</sub>: 0–10%
- H<sub>2</sub>S: 0–2% (can be higher in some cases)[30]

### III.3.1.4. Flue Gas (Combustion Exhaust)

From burning fossil fuels (e.g., coal, natural gas):

- N<sub>2</sub>: 70–75%
- CO<sub>2</sub>: 5–15%
- H<sub>2</sub>O: 5–10%
- O<sub>2</sub>: 2–10%
- CO: <1% (depends on combustion efficiency)
- SO<sub>2</sub>/NO<sub>x</sub>: Trace to ppm levels[70]

#### **III.3.1.5. Coal Gas (Town Gas, Historical)**

Produced from coal gasification (historically used for lighting/heating):

- H<sub>2</sub>: 30–50%
- CH<sub>4</sub>: 15–30%
- CO: 10–20%
- CO<sub>2</sub>: 5–10%
- [71]N<sub>2</sub>: 5–15%

#### **III.3.1.6. Blast Furnace Gas (Steel Industry Byproduct)**

- CO: 20–30%
- CO<sub>2</sub>: 15–25%
- N<sub>2</sub>: 50–55%
- H<sub>2</sub>: 1–5%

### **III.3.2. Pollutant gas content (HCl, SO<sub>2</sub>, NO<sub>x</sub>, etc.)**

#### **III.3.2.1. Hydrogen Chloride (HCl)**

**III.3.2.1. a. Sources: Waste incineration, coal combustion, chemical manufacturing.**

#### **III.3.2.1. b. Typical Concentrations:**

- Coal-fired power plants: 10–200 ppm (US EPA, 2022).[72]
- Municipal waste incineration: 100–1000 ppm (European Environment Agency, 2020).

**III.3.2.1.c. Health/Environmental Impact: Corrosive, contributes to acid rain.[73]**

**III.3.2.2. Sulfur Dioxide (SO<sub>2</sub>)**

**III.3.2.2.a. Sources: Fossil fuel combustion (coal, oil), smelting.[74]**

**III.3.2.2.b. Typical Concentrations:**

- Coal power plants: 50–1000 ppm (IPCC, 2006).
- Global ambient levels: 0.1–20 ppb [73].

**III.3.2.2.c. Health/Environmental Impact: Respiratory issues, acid rain precursor.**

**III.3.2.3. Nitrogen Oxides (NO<sub>x</sub> = NO + NO<sub>2</sub>)**

III.3.2.3.a. Sources: Vehicle emissions, power plants, industrial combustion.

III.3.2.3.b. Typical Concentrations:

- Diesel exhaust: 100–1000 ppm (EPA, 2023).
- Urban ambient air: 10–200 ppb [73].

III.3.2.3.c. Health/Environmental Impact: Smog, ozone depletion, respiratory diseases.

**III.3.2.4. Carbon Monoxide (CO)**

III.3.2.4.a. Sources: Incomplete combustion (vehicles, wildfires).

III.3.2.4.b. Typical Concentrations:

- Vehicle exhaust: 1,000–50,000 ppm (EPA, 2023).[75]
- Urban areas: 0.5–10 ppm [73].

III.3.2.4.c. Health Impact: Binds to hemoglobin, causing hypoxia.

**III.3.2.5. Particulate Matter (PM<sub>2.5</sub>, PM<sub>10</sub>)**

III.3.2.5.a. Sources: Combustion, dust, industrial processes.

III.3.2.5.b. Typical Concentrations:

- Heavy traffic areas: 20–100 µg/m<sup>3</sup> (PM<sub>2.5</sub>) [110].

○ Coal plants: 5–50 mg/m<sup>3</sup> [73]. The calorific value of a gas refers to the amount of energy released when a specific volume of gas is completely combusted under standard conditions. It is typically expressed in megajoules per cubic meter (MJ/m<sup>3</sup>) or British Thermal Units per cubic foot (BTU/ft<sup>3</sup>).

### III.3.2.6. There are two types of calorific values:

III.3.2.6.a. Higher Calorific Value (HCV) or Gross Calorific Value (GCV): Includes the heat recovered from condensing water vapor in the combustion products.

III.3.2.6.b. Lower Calorific Value (LCV) or Net Calorific Value (NCV): Excludes the latent heat of vaporization of water in the combustion products.

**Table 10: Typical Calorific Values of Common Gases**

Gas	Higher Calorific Value (GCV)	Lower Calorific Value (NCV)	References
Natural Gas	~37–43 MJ/m <sup>3</sup> (~1,000–1,150 BTU/ft <sup>3</sup> )	~34–39 MJ/m <sup>3</sup> (~900–1,050 BTU/ft <sup>3</sup> )	[77][78]
Methane (CH <sub>4</sub> )	55.5 MJ/kg (~37.8 MJ/m <sup>3</sup> )	50.0 MJ/kg (~34.0 MJ/m <sup>3</sup> )	[79][80]
Propane (C <sub>3</sub> H <sub>8</sub> )	93.2 MJ/m <sup>3</sup> (~2,516 BTU/ft <sup>3</sup> )	85.8 MJ/m <sup>3</sup> (~2,320 BTU/ft <sup>3</sup> )	[81][82]
Butane (C <sub>4</sub> H <sub>10</sub> )	121.8 MJ/m <sup>3</sup> (~3,300 BTU/ft <sup>3</sup> )	111.4 MJ/m <sup>3</sup> (~3,000 BTU/ft <sup>3</sup> )	[83][84]
Hydrogen (H <sub>2</sub> )	141.8 MJ/kg (~12.7 MJ/m <sup>3</sup> )	120.0 MJ/kg (~10.8 MJ/m <sup>3</sup> )	[85][86]
Biogas (60% CH <sub>4</sub> )	~22–26 MJ/m <sup>3</sup> (~600–700 BTU/ft <sup>3</sup> )	~20–24 MJ/m <sup>3</sup> (~550–650 BTU/ft <sup>3</sup> )	[86][87]

## III.4. Analysis of Residual Ashes

### III.4.1. Chemical composition of ashes

The chemical composition of ashes depends on the source material (e.g., wood, coal, plant matter, or industrial waste) and combustion conditions. Below is a general breakdown of the chemical composition of different types of ashes with references:

#### **III.4.1.1. Wood Ash**

Wood ash is primarily composed of metal carbonates, oxides, and hydroxides, with calcium (Ca) being the dominant element.[88][89]

Typical composition (dry basis, % by weight):

- CaO (Calcium oxide): 25–45%
- K<sub>2</sub>O (Potassium oxide): 2–10%
- MgO (Magnesium oxide): 1–5%
- P<sub>2</sub>O<sub>5</sub> (Phosphorus pentoxide): 0.5–2%
- SiO<sub>2</sub> (Silicon dioxide): 5–20%
- Al<sub>2</sub>O<sub>3</sub> (Aluminum oxide): 1–5%
- Fe<sub>2</sub>O<sub>3</sub> (Iron oxide): 0.5–2%
- Na<sub>2</sub>O (Sodium oxide): 0.1–2%
- SO<sub>3</sub> (Sulfur trioxide): 0.1–1%

#### **III.4.1.2. Coal Fly Ash**

Coal ash is classified into fly ash (fine particles from flue gases) and bottom ash (coarser residue). Fly ash is rich in silica, alumina, and iron oxides. Typical composition (% by weight)[90][91]:

- SiO<sub>2</sub>: 40–60%
- Al<sub>2</sub>O<sub>3</sub>: 20–30%
- Fe<sub>2</sub>O<sub>3</sub>: 5–15%
- CaO: 1–10% (higher in Class C fly ash)
- MgO: 0.5–4%
- K<sub>2</sub>O & Na<sub>2</sub>O: 1–4%

- SO<sub>3</sub>: 0.2–5%
- Unburned carbon (LOI): 0.5–10%

#### **III.4.1.3. Biomass Ash (Agricultural Residues)**

Biomass ash from crop residues (e.g., rice husk, straw) has high silica content. Example (Rice Husk Ash, % by weight)[92]:

- SiO<sub>2</sub>: 85–95%
- K<sub>2</sub>O: 1–5%
- CaO: 0.5–3%
- MgO: 0.2–1%
- P<sub>2</sub>O<sub>5</sub>: 0.5–3%

#### **III.4.1.4. Municipal Solid Waste (MSW) Ash**

MSW incineration ash contains a mix of metals, silicates, and chlorides. Typical composition (% by weight)[93]:

- SiO<sub>2</sub>: 20–40%
- CaO: 10–30%
- Al<sub>2</sub>O<sub>3</sub>: 5–15%
- Fe<sub>2</sub>O<sub>3</sub>: 5–10%
- Na<sub>2</sub>O & K<sub>2</sub>O: 2–8%
- Heavy metals (Pb, Cd, Zn, Cu): 0.1–2%

#### **III.4.1.5. Volcanic Ash**

Volcanic ash is rich in silicates and varies based on eruption chemistry. Typical composition (% by weight)[94]:

- SiO<sub>2</sub>: 45–75%
- Al<sub>2</sub>O<sub>3</sub>: 10–20%
- FeO/Fe<sub>2</sub>O<sub>3</sub>: 5–15%

- CaO: 5–10%
- MgO: 1–5%
- Na<sub>2</sub>O & K<sub>2</sub>O: 1–10%

### **III.4.2. Morphological characterization of ashes**

The morphological characterization of ashes involves studying their physical structure, particle shape, size distribution, surface texture, and porosity using various analytical techniques. These properties influence the ash's reactivity, disposal, and potential utilization in construction, agriculture, and environmental applications. Below is a detailed discussion with key references.

#### **III.4.2.1. Particle Shape and Size Distribution**

Ash particles can vary in shape (spherical, irregular, angular) and size (from fine powders to coarse fragments), depending on the source material and combustion conditions.

- Fly ash (from coal combustion) typically consists of spherical particles (cenospheres and plerospheres) due to rapid cooling in flue gases [95].
- Biomass ash often contains irregular, porous, and elongated particles due to organic residues (Thy et al., 2013).
- Bottom ash is coarser and more angular due to slower cooling in the furnace.

Analytical Techniques:

- Scanning Electron Microscopy (SEM) – Provides high-resolution images of particle morphology (Sarbak & Kramer-Wachowiak, 2002).
- Laser Diffraction – Measures particle size distribution [95].

#### **III.4.2.2. Surface Texture and Porosity**

Ash surfaces can be smooth, vesicular (porous), or rough, affecting their adsorption capacity and reactivity.[95]

- Coal fly ash has a glassy, smooth surface due to vitrification [98].
- Biomass ash tends to be more porous due to unburned carbon and cellular structures [96].

Analytical Techniques:

- Brunauer-Emmett-Teller (BET) Analysis – Quantifies surface area and porosity [97].
- Mercury Intrusion Porosimetry (MIP) – Measures pore size distribution.

#### **III.4.2.3. Chemical Composition and Phase Analysis**

Morphology is influenced by chemical composition ( $\text{SiO}_2$ ,  $\text{Al}_2\text{O}_3$ ,  $\text{CaO}$ ,  $\text{Fe}_2\text{O}_3$ , etc.) and mineral phases (crystalline vs. amorphous).

- High-calcium ashes (e.g., from wood or municipal waste) form more irregular, reactive particles [98].

- Silica-rich ashes (e.g., rice husk ash) have a highly porous, nanostructured morphology [100].

Analytical Techniques:

- X-ray Diffraction (XRD) – Identifies crystalline phases [98].
- Energy-Dispersive X-ray Spectroscopy (EDS) – Provides elemental mapping [97].

#### **III.4.2.4. Applications Based on Morphology**

- Cementitious materials (smooth, spherical fly ash improves workability) [97].
- Adsorbents (porous biomass ash for heavy metal removal) [100].
- Geopolymers (amorphous, reactive ash enhances strength).

### **III.5. Material and Energy Balance of Gasification**

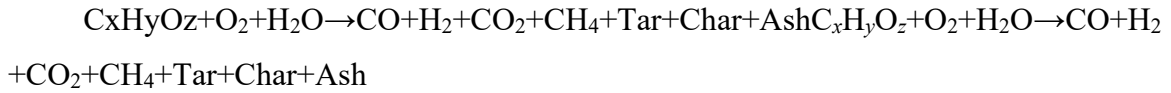
Gasification is a thermochemical process that converts carbonaceous materials (e.g., coal, biomass, waste) into a gaseous product called syngas (primarily  $\text{CO}$ ,  $\text{H}_2$ ,  $\text{CH}_4$ , and  $\text{CO}_2$ ) by reacting the feedstock at high temperatures ( $700\text{--}1500^\circ\text{C}$ ) with a controlled amount of oxygen, steam, or air.

To analyze gasification processes, material and energy balances are essential for understanding efficiency, optimizing conditions, and scaling up the process.

#### **III.5.1. Material Balance**

The material balance ensures that the mass inputs equal the mass outputs, accounting for all components in the process.

### III.5.1.1 General Gasification Reaction:



#### III.5.1.1.a. Inputs:

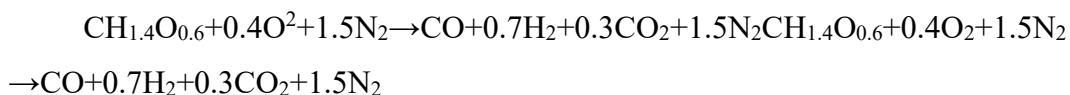
1. Feedstock (Biomass/Coal/Waste) – Contains carbon (C), hydrogen (H), oxygen (O), nitrogen (N), sulfur (S), and ash.
2. Gasifying Agent – Air ( $O_2 + N_2$ ), oxygen ( $O_2$ ), or steam ( $H_2O$ ).
3. Additional Inputs (if any) – Catalysts, additives.

#### III.5.1.1.b. Outputs:

1. Syngas (Producer Gas) – CO,  $H_2$ ,  $CH_4$ ,  $CO_2$ .
2. Tar – Condensable hydrocarbons.
3. Char/Unburnt Carbon – Solid residue.
4. Ash/Slag – Inorganic residue.
5. Water Vapor – From moisture and reactions.

#### III.5.1.1.c. Stoichiometric Example (Biomass Gasification):

#### III.5.1.1.d. For a simplified biomass formula ( $CH_{1.4}O_{0.6}$ ) gasified with air:



*(Balanced based on elemental composition)*

#### Key Parameters:

- Equivalence Ratio (ER) = (Actual air supplied) / (Stoichiometric air required)[101]
- Carbon Conversion Efficiency (CCE) = (Carbon in syngas) / (Carbon in feedstock) × 100%

### III.5.2. Energy Balance

The energy balance ensures that the energy input (from feedstock and gasifying agent) equals energy output (syngas, heat losses, etc.)[102].

### III.5.2.1 Energy Inputs:

1. Heating Value of Feedstock – Higher Heating Value (HHV) or Lower Heating Value (LHV)[103].
2. Sensible Heat – Heat from gasifying agent (if preheated).
3. Heat from Reactions – Exothermic reactions (oxidation) contribute energy.

### III.5.2.2 Energy Outputs:

1. Syngas Heating Value – LHV or HHV of produced gas[104].
2. Sensible Heat in Syngas – Energy due to gas temperature.
3. Heat Losses – Radiation, convection, unburnt carbon, tar.
4. Heat for Endothermic Reactions – Steam reforming, Boudouard reaction.

### III.5.2.3 Energy Efficiency Metrics:

- Cold Gas Efficiency (CGE) =  $(\text{Energy in syngas}) / (\text{Energy in feedstock}) \times 100\%$
- Hot Gas Efficiency (HGE) = Includes sensible heat of syngas[105].

### III.5.2.4 Example Calculation:

If biomass (LHV = 18 MJ/kg) is gasified to produce syngas (LHV = 5 MJ/Nm<sup>3</sup>) at a yield of 2.5 Nm<sup>3</sup>/kg:

$$\text{CGE} = \frac{5 \times 2.5}{18} \times 100\% \approx 69.4\% \quad \text{CGE} = \frac{185}{185} \times 2.5 \times 100\% \approx 69.4\%$$

The performance of any gasification process is largely dictated by the type and design of the gasifier employed. Each gasifier offers distinct operational benefits and constraints, making proper selection crucial for achieving desired energy outputs and minimizing environmental harm. Continued innovation in gasifier technology—alongside tailored process control—will be essential for scaling up gasification solutions and adapting them to increasingly complex waste streams.

**Chapter IV**

**Economic and  
Environmental Aspects of  
Valorizing Organic Waste  
through Gasification.**

While gasification holds significant technological promise, its long-term adoption depends heavily on both its economic viability and environmental performance. Evaluating the costs, benefits, and trade-offs of this technology is essential for determining its role in sustainable development and waste management strategies. This chapter examines the economic drivers and barriers to implementation, such as capital investment, operational costs, and market incentives. It also explores the environmental implications of gasification, including emissions, residue handling, and potential for greenhouse gas mitigation.

#### IV.1. Cost Analysis of the Gasification Process

##### IV.1.1. Initial investment

The term "**initial investment**" refers to the upfront capital required to start a project, business, or investment. It includes costs such as equipment, land, inventory, research & development (R&D), and other startup expenses. Below is a breakdown with references:

##### IV.1.1.1. Components of Initial Investment

1. Fixed Assets – Machinery, buildings, vehicles, etc.
2. Working Capital – Cash needed for daily operations (inventory, salaries, rent).
3. Pre-operational Expenses – Licenses, permits, market research.
4. Research & Development (R&D) – Product testing, prototyping.
5. Marketing & Branding – Advertising, website development.

**Table 11:** Example Calculation

Item	Cost (\$)
Machinery & Equipment	100,000
Office Setup	20,000
Initial Inventory	30,000
Marketing & Branding	15,000

Item	Cost (\$)
Legal & Licensing Fees	5,000
Total Initial Investment	170,000

1. Investopedia – Defines initial investment as the capital required to start a business or project.

Investopedia - Initial Investment

2. Harvard Business Review – Discusses startup costs and capital budgeting.

3. U.S. Small Business Administration (SBA) – Provides guidelines on calculating startup costs.

4. SBA - Startup Costs

#### IV.1.2. Operating costs

Operating costs, also known as operating expenses (OPEX), are the ongoing expenses incurred from the normal day-to-day operations of a business. These costs are essential for maintaining business operations and generating revenue. Below is a breakdown of common operating costs with references to authoritative sources:

##### IV.1.2.1. Types of Operating Costs

**Operating costs can be categorized into:**

###### a) Fixed Costs

- Expenses that remain constant regardless of production or sales volume.
  - Rent or lease payments
  - Salaries and wages (for non-production staff)
  - Insurance premiums
  - Depreciation and amortization
  - Utilities (base charges)

**b) Variable Costs**

- Expenses that fluctuate with production or sales volume.
  - Raw materials and supplies
  - Direct labor (production workers)
  - Sales commissions
  - Shipping and distribution costs
  - Utility costs tied to production (e.g., electricity for manufacturing)

**c) Semi-Variable Costs**

- Expenses with both fixed and variable components.
  - Phone/internet bills (fixed base + variable usage)
  - Maintenance and repairs
  - Overtime wages

**IV.1.2.2.Importance of Operating Costs**

- Profitability Analysis: Operating costs directly impact gross and net profit margins.
- Budgeting & Cost Control: Helps businesses optimize spending.
- Investor & Lender Evaluation: Key metric in financial statements (Income Statement).

**IV.1.2.3.Calculation of Operating Costs****The formula for operating costs is:**

Operating Costs=Cost of Goods Sold (COGS)+Operating Expenses (OPEX)  
Operating Costs=Cost of Goods Sold (COGS)+Operating Expenses (OPEX)

Where:

- COGS = Direct costs of producing goods (materials, labor).
- OPEX = Indirect costs (rent, salaries, marketing).

1. Investopedia – "Operating costs are associated with the maintenance and administration of a business on a day-to-day basis."

- Investopedia - Operating Costs
- 2. Corporate Finance Institute (CFI) – "Operating expenses include rent, equipment, inventory costs, marketing, payroll, insurance, and R&D."
- CFI - Operating Expenses
- 3. AccountingTools – "Operating costs are the expenses a business incurs through normal operations."
- AccountingTools - Operating Costs
- 4. U.S. Securities and Exchange Commission (SEC) – Public companies must report operating expenses in financial filings (10-K, 10-Q).
- SEC.gov
- 5. Reducing Operating Costs
  - Automating processes
  - Outsourcing non-core functions
  - Negotiating supplier contracts
  - Energy efficiency improvements

#### **IV.1.3.Revenues from the sale of energy or chemical products**

Revenues from the sale of energy or chemical products can come from a variety of sources, including oil, natural gas, refined petroleum products, petrochemicals, specialty chemicals, and renewable energy products. Below are key references and examples of companies and industries involved in these sectors:

##### **IV.1.3.1. Oil & Gas (Upstream, Midstream, Downstream)**

- Crude Oil & Natural Gas Sales: Major oil companies like Saudi Aramco, ExxonMobil, Chevron, BP, Shell, and TotalEnergies generate significant revenue from hydrocarbon sales.
- Refined Products: Gasoline, diesel, jet fuel, and lubricants sold by refiners like Valero Energy, Marathon Petroleum, and Reliance Industries.
- LNG (Liquefied Natural Gas): Companies like Cheniere Energy, QatarEnergy, and Shell profit from LNG exports.

- BP Statistical Review of World Energy
- OPEC Annual Report

#### **IV.1.3.2. Petrochemicals & Basic Chemicals**

• Ethylene, Propylene, Methanol, Benzene: Sold by companies like Dow Chemical, BASF, SABIC, LyondellBasell, and Sinopec.

• Fertilizers (Ammonia, Urea, Potash): Key players include Nutrien, Yara International, and CF Industries.

- American Chemistry Council (ACC) Reports
- ICIS Chemical Business

#### **IV.1.3.3. Specialty Chemicals & Advanced Materials**

• Polymers, Coatings, Adhesives: Companies like 3M, DuPont, and AkzoNobel.

• Lithium, Rare Earth Metals: Used in batteries; suppliers include Albemarle, Livent, and Lynas Rare Earths.[106]

- McKinsey Chemicals Insights[107]

#### **IV.1.3.4. Renewable Energy & Biofuels**

• Solar & Wind Energy: Companies like NextEra Energy, Ørsted, and Vestas.

• Biofuels (Ethanol, Biodiesel): Producers like POET, ADM, and Neste.

• Hydrogen & Green Chemicals: Emerging players like Plug Power, Air Products, and Linde.

#### **IV.1.3.5. Trading & Commodity Markets**

• Companies like Glencore, Trafigura, Vitol, and Cargill trade energy and chemical products globally.

- Prices are influenced by benchmarks like Brent Crude, WTI, and Platts Assessments.
- Platts (S&P Global Commodity Insights)
- ICE (Intercontinental Exchange) Futures.

## IV.2.Environmental Impact Analysis of the Gasification Process

### IV.2.1.Greenhouse gas emissions

Greenhouse gas (GHG) emissions are gases that trap heat in the Earth's atmosphere, contributing to the greenhouse effect and global warming. The primary GHGs include carbon dioxide (CO<sub>2</sub>), methane (CH<sub>4</sub>), nitrous oxide (N<sub>2</sub>O), and fluorinated gases (such as hydrofluorocarbons, HFCs). Here's an overview of key sources and trends, supported by scientific references:

#### IV.2.1.1.Major Greenhouse Gases and Their Sources

##### a) Carbon Dioxide (CO<sub>2</sub>)

- Sources: Burning fossil fuels (coal, oil, natural gas) for energy, deforestation, and industrial processes (e.g., cement production)[110].
- Contribution: Accounts for ~76% of global GHG emissions.

##### b) Methane (CH<sub>4</sub>)

- Sources: Livestock (enteric fermentation), rice paddies, fossil fuel extraction, landfills, and natural gas leaks.
- Global Warming Potential (GWP): 28–36 times more potent than CO<sub>2</sub> over 100 years[108].

##### c) Nitrous Oxide (N<sub>2</sub>O)

- Sources: Agricultural fertilizers, manure management, fossil fuel combustion, and industrial processes.
- GWP: ~265–298 times more potent than CO<sub>2</sub> over 100 years [109].

##### d) Fluorinated Gases (F-gases)

- Sources: Refrigerants (HFCs), semiconductor manufacturing, and insulating gases (SF<sub>6</sub>).[110]
- GWP: Thousands of times more potent than CO<sub>2</sub>.
  - UNEP (2020). *Emissions Gap Report 2020*. Link

#### IV.2.1.2. Sector-Wise Contributions

##### According to the World Resources Institute (WRI):

- Energy (73.2%): Electricity/heat production, transportation, manufacturing[111].
- Agriculture (18.4%): Livestock, soil management, rice cultivation[112].
- Industry (5.2%): Cement, chemicals, metal production.
- Waste (3.2%): Landfills, wastewater.
- WRI (2021). *Climate Watch*. Link

#### IV.2.1.3. Recent Trends

- Global CO<sub>2</sub> emissions reached 36.8 billion metric tons in 2022 [106].
- Methane emissions have risen sharply due to oil/gas leaks and agriculture

#### IV.2.1.4. Mitigation Strategies

- Transition to renewable energy (solar, wind).
- Carbon capture and storage (CCS).
- Methane leak reduction in oil/gas.
- Sustainable agriculture practices.

#### IV.2.2. Pollutant releases into air, water, and soil

Pollutant releases into air, water, and soil are significant environmental concerns, contributing to pollution, ecosystem degradation, and public health risks. Below is an overview of major pollutants released into these media, along with key references from authoritative sources.

##### IV.2.2.1. Air Pollutants

Air pollution results from both natural and anthropogenic sources, with the latter being the primary concern due to industrialization, transportation, and energy production.

Major Air Pollutants:

- Particulate Matter (PM<sub>2.5</sub> and PM<sub>10</sub>): Tiny particles from vehicle exhaust, industrial emissions, and wildfires.
- Nitrogen Oxides (NO<sub>x</sub>): Emitted from combustion processes (e.g., vehicles, power plants), contributing to smog and acid rain.
- Sulfur Dioxide (SO<sub>2</sub>): Released from burning fossil fuels, leading to respiratory issues and acid rain.
- Volatile Organic Compounds (VOCs): From industrial solvents, paints, and fuels, contributing to ozone formation.
- Carbon Monoxide (CO) & Carbon Dioxide (CO<sub>2</sub>): CO is a toxic gas from incomplete combustion, while CO<sub>2</sub> is a major greenhouse gas .

#### IV.2.2.2 Water Pollutants

Water pollution arises from industrial discharges, agricultural runoff, and improper waste disposal.

##### **Major Water Pollutants:**

- Heavy Metals (Lead, Mercury, Arsenic): From industrial effluents and mining.
- Nutrients (Nitrates & Phosphates): From agricultural runoff, causing eutrophication.
- Organic Pollutants (Pesticides, PCBs): Persistent chemicals that bioaccumulate in aquatic life [113].
- Microplastics: From plastic waste breakdown, affecting marine ecosystems.
- Pathogens (E. coli, Giardia): From sewage discharge, causing waterborne diseases.

#### IV.2.2.3. Soil Pollutants

Soil contamination affects agriculture, groundwater, and ecosystems.

##### **Major Soil Pollutants:**

- Heavy Metals (Cadmium, Lead): From industrial waste and pesticides.
- Petroleum Hydrocarbons: From oil spills and leaks.
- Pesticides & Herbicides: Long-term residues affect soil health.

- Industrial Chemicals (Dioxins, PCBs): Persistent organic .
- Salts & Acidifying Agents: From improper irrigation and acid rain.

### IV.2.3.Comparison with other organic waste valorization processes

Organic waste valorization encompasses various technologies aimed at converting waste into valuable products like energy, fertilizers, and chemicals. Below is a comparison of key organic waste valorization processes, including anaerobic digestion (AD), composting, pyrolysis, gasification, and hydrothermal carbonization (HTC), with references to relevant studies.

#### IV.2.3.1.Anaerobic Digestion (AD)

- Process: Microbial breakdown of organic matter in the absence of oxygen, producing biogas ( $\text{CH}_4 + \text{CO}_2$ ) and digestate.

- **Advantages:**

- High energy recovery as biogas (50–70% methane) [113].
- Digestate can be used as fertilizer.
- Suitable for wet waste (e.g., food waste, manure).

- **Limitations:**

- Slow process (weeks to months).
- Sensitive to feedstock composition (e.g., inhibitors like ammonia).

#### IV.2.3.2.Composting

- Process: Aerobic decomposition of organic waste into stable compost.

- **Advantages:**

- Low-cost and simple technology.
- Produces nutrient-rich soil amendment.

- **Limitations:**

- Greenhouse gas emissions ( $\text{CO}_2$ ,  $\text{CH}_4$ ,  $\text{N}_2\text{O}$ ).

- Limited to solid organic waste (e.g., yard waste).

#### IV.2.3.3. Pyrolysis

• Process: Thermal decomposition at 300–800°C in absence of oxygen, yielding biochar, bio-oil, and syngas.

• **Advantages:**

- High-value products (biochar for soil improvement, bio-oil for fuel) (Bridgwater, 2012).[114]
- Handles diverse feedstocks (e.g., lignocellulosic waste).

• **Limitations:**

- High energy input required.
- Bio-oil requires upgrading.

#### IV.2.3.4. Gasification

• Process: Partial oxidation at high temperatures (700–1200°C) to produce syngas (CO + H<sub>2</sub>).

• **Advantages:**

- Syngas can be used for electricity or chemical synthesis [115].
- Higher efficiency than incineration.

• **Limitations:**

- Tar formation complicates syngas cleaning.
- High capital costs.

#### IV.2.3.5. Hydrothermal Carbonization (HTC)

• Process: Converts wet waste into hydrochar at 180–250°C under pressure.

• **Advantages:**

- No drying required (ideal for food waste, sewage sludge).
- Hydrochar has high energy density [116].

- **Limitations:**

- High-pressure reactors increase costs.[116]
- Limited scalability.

**Table 12:** Comparison Summary

Process	Products	Energy Efficiency	Suitable Feedstock	Key Challenges
AD	Biogas, digestate	Moderate (40–60%)	Food waste, manure	Slow, sensitive to toxins
Composting	Compost	Low (no energy rec.)	Yard waste, solids	GHG emissions
Pyrolysis	Biochar, bio-oil, syngas	High (60–75%)	Dry biomass	High energy input
Gasification	Syngas	High (50–70%)	Mixed organic waste	Tar formation
HTC	Hydrochar	Moderate (50–65%)	Wet waste	High-pressure reactors

Gasification offers a compelling combination of economic potential and environmental benefit, particularly when integrated into broader waste valorization strategies. Though the initial costs can be high, long-term savings, energy recovery, and reduced landfill use often offset these expenses. Environmentally, gasification can significantly lower harmful emissions compared to incineration, especially when equipped with advanced cleanup technologies. Moving forward, supportive policy frameworks and technological improvements will be key to maximizing the economic and ecological value of gasifying organic waste.

# Conclusion

## Conclusion

The gasification of organic waste presents a promising pathway for sustainable waste management and energy recovery, offering significant environmental and economic benefits. As global concerns over waste accumulation, greenhouse gas emissions, and energy security intensify, gasification technology stands out as a viable solution to convert organic waste into syngas, biofuels, and other valuable byproducts.

### Key Advantages:

1. Waste Reduction & Circular Economy – Gasification helps divert organic waste from landfills, reducing methane emissions and promoting resource efficiency.
2. Renewable Energy Production – Syngas generated can be used for electricity, heat, or further processed into hydrogen and biofuels, supporting decarbonization efforts.
3. Lower Environmental Impact – Compared to incineration, gasification operates with higher efficiency and lower emissions when optimized properly.
4. Flexibility in Feedstock – The technology can process diverse organic wastes, including agricultural residues, food waste, and sewage sludge.

### Challenges & Barriers:

1. High Initial Costs & Technology Complexity – Capital-intensive setups and operational challenges hinder widespread adoption.
2. Feedstock Variability & Pre-Treatment Needs – Inconsistent waste composition requires sorting and drying, increasing processing costs.
3. Regulatory & Market Hurdles – Policies often favor conventional waste management, and incentives for gasification projects remain limited in many regions.
4. Public Acceptance & Perception – Misconceptions about emissions and safety can slow project approvals.

### Future Outlook:

The development of gasification technology for organic waste depends on:

- Technological Advancements (improved efficiency, lower costs, and better emission controls).

## Conclusion

---

- Stronger Policy Support (subsidies, carbon pricing, and waste-to-energy mandates).
- Public-Private Partnerships (scaling up pilot projects to commercial viability).
- Integration with Other Renewable Systems (e.g., combining gasification with carbon capture for negative emissions).

This dissertation has explored the multifaceted nature of organic waste and the technological advancements aimed at its effective valorization. Beginning with an overview of organic waste sources and types, the study highlighted the importance of characterizing waste materials to inform suitable treatment options. The gasification process, examined in depth, emerges as a viable solution for converting organic waste into energy-rich syngas, offering both environmental and economic benefits. Central to this process is the gasifier itself, whose design and operational efficiency play a crucial role in determining output quality. Furthermore, the economic and environmental evaluation of waste vaporization through gasification reinforces its potential as a sustainable alternative to conventional waste disposal methods.

Ultimately, managing organic waste through advanced thermochemical techniques not only contributes to cleaner energy production but also supports broader goals of environmental protection and resource circularity. Continued research, investment, and policy support will be essential for integrating these solutions at larger scales and ensuring their long-term viability in a world increasingly shaped by sustainability imperatives.

# References

## References

- [1] Loha, C., Chattopadhyay, H., & Chatterjee, P. K. (2014). Performance of fixed bed gasifier fueled with agro-residues. *Energy Conversion and Management*, 87, 359–365.
- [2] McKendry, P. (2002). *Energy production from biomass (part 2): Conversion technologies*. *Bioresource Technology*, 83(1), 55–63.
- [3] Bridgwater, A. V. (2003). *Renewable fuels and chemicals by thermal processing of biomass*. *Chemical Engineering Journal*, 91(2–3), 87–102.
- [4] Kumar, A., Jones, D. D., & Hanna, M. A. (2009). *Thermochemical biomass gasification: A review*. *Energy & Fuels*, 23(3), 1473–1485.
- [5] Zhou, C., Bai, H., & Wang, W. (2009). *Effect of temperature on biomass gasification*. *Journal of Renewable Energy*, 34(6), 1452–1458.
- [6] Arena, U. (2012). *Process and technological aspects of municipal solid waste gasification*. *Waste Management*, 32(4), 625–639.
- [7] Ptasiński, K. J., Prins, M. J., & Pierik, A. (2007). *Exergetic evaluation of biomass gasification*. *Energy*, 32(4), 568–574.
- [8] Basu, P. (2010). *Biomass Gasification and Pyrolysis: Practical Design and Theory*. Academic Press.
- [9] Heidenreich, S., & Foscolo, P. U. (2015). *Advanced biomass gasification*. *Progress in Energy and Combustion Science*, 46, 72–95.
- [10] Materazzi, M., Lettieri, P., & Taylor, R. (2016). *CO<sub>2</sub> as a gasifying agent in advanced waste conversion*. *Energy Conversion and Management*, 118, 13–27.
- [11] Knoef, H. (Ed.). (2012). *Handbook of Biomass Gasification*. BTG Biomass Technology Group.
- [12] Sutton, D., Kelleher, B., & Ross, J. R. H. (2001). *Review of literature on catalysts for biomass gasification*. *Fuel Processing Technology*, 73(3), 155–173.
- [13] Higman, C., & van der Burgt, M. (2008). *Gasification* (2nd ed.). Gulf Professional Publishing.

- [14] Reed, T. B., & Das, A. (1988). *Handbook of Biomass Downdraft Gasifier Engine Systems*. Solar Energy Research Institute.
- [15] Bridgwater, A. V. (2012). *Review of fast pyrolysis of biomass and product upgrading. Biomass and Bioenergy*, 38, 68–94.
- [16] Mohan, D., Pittman Jr., C. U., & Steele, P. H. (2006). *Pyrolysis of wood/biomass for bio-oil: A critical review. Energy & Fuels*, 20(3), 848–889.
- [17] Zhang, X., Lei, H., Chen, S., & Wu, J. (2016). *Catalytic co-pyrolysis of lignocellulosic biomass with polymers: A review. Green Chemistry*, 18(15), 4145–4169.
- [18] Lehmann, J., & Joseph, S. (2015). *Biochar for Environmental Management: Science, Technology and Implementation* (2nd ed.). Routledge.
- [19] Butler, E., Devlin, G., Meier, D., & McDonnell, K. (2011). *A review of recent laboratory research and commercial developments in fast pyrolysis and upgrading. Renewable and Sustainable Energy Reviews*, 15(8), 4171–4186.
- [20] Makarichi, L., Jutidamrongphan, W., & Techato, K. (2018). *The evolution of waste-to-energy incineration: A review. Renewable and Sustainable Energy Reviews*, 91, 812–821.
- [21] EPA. *Waste Incineration Guidelines*. United States Environmental Protection Agency.
- [22] Weiland, P. (2010). *Biogas production: Current state and perspectives. Applied Microbiology and Biotechnology*, 85, 849–860.
- [23] Appels, L., Baeyens, J., Degreè, J., & Dewil, R. (2011). *Principles and potential of the anaerobic digestion of waste-activated sludge. Renewable and Sustainable Energy Reviews*, 15(1), 4295–4301.
- [24] Pandey, A., Larroche, C., Dussap, C. G., & Gnansounou, E. (2015). *Advances in bioprocessing of renewable resources for fuels and chemicals*. Elsevier.
- [25] Hoornweg, D., & Bhada-Tata, P. (2012). *What a Waste: A Global Review of Solid Waste Management*. World Bank.
- [26] International Energy Agency (IEA). (2021). *Hydrogen from Renewable Resources: Global Status Report*.

## References

---

- [27] Appels et al. (2008) provide a foundational understanding of the biological and engineering principles underlying anaerobic digestion processes
- [28] Gerardi (2003) describes the microbiology of anaerobic digesters in detail, emphasizing the role of microbial communities in stabilizing the digestion process
- [29] Mao et al. (2015) reviewed recent achievements in biogas technology and identified key optimization parameters for anaerobic digestion systems
- [30] Appels, L., Baeyens, J., Degève, J., & Dewil, R. (2008). Principles and potential of anaerobic digestion of waste-activated sludge. *Progress in Energy and Combustion Science*, 34(6), 755–781.
- [31] Gerardi, M. H. (2003). *The microbiology of anaerobic digesters*. John Wiley & Sons.
- [32] Mao, C., Feng, Y., Wang, X., & Ren, G. (2015). Review on research achievements of biogas from anaerobic digestion. *Renewable and Sustainable Energy Reviews*, 45, 540–555.
- [33] Basu, P. (2013). *Biomass Gasification, Pyrolysis, and Torrefaction* (2nd ed.). Academic Press.
- [34] Hofbauer, H., et al. (2002). "The FICFB Gasification Process." *Biomass and Bioenergy*, 23(6), 395-403.
- [35] Liu, H., et al. (2011). "Entrained Flow Gasification of Biomass." *Energy & Fuels*, 25(7), 2944-2952.
- [36] Gomez, E., et al. (2009). "Thermal Plasma Treatment of Waste." *Waste Management*, 29(5), 1393-1409.
- [37] Matsumura, Y., et al. (2005). "Biomass Gasification in Supercritical Water." *Industrial & Engineering Chemistry Research*, 44(5), 1119-1129
- [38] Basu, P. (2010). *Biomass Gasification and Pyrolysis*. Academic Press.
- [39] Bridgwater, A. V. (2003). *Renewable and Sustainable Energy Reviews*, 7(3), 1–73.
- [40] McKendry, P. (2002). *Bioresource Technology*, 83(1), 37–46.
- [41] Higman, C., & van der Burgt, M. (2008). *Gasification*. Elsevier.

## References

---

- [42]Matsumoto, K., et al. (2019). *Fuel*, 236, 980–986.
- [43]Heberlein, J., & Murphy, A. B. (2008). *Journal of Physics D: Applied Physics*, 41(5).
- [44]Molino, A., et al. (2016). "Biomass gasification technology: The state of the art overview." *Journal of Energy Chemistry*, 25(1), 10-25.
- [45] Puig-Arnabat, M., et al. (2010). "Review and analysis of biomass gasification models." *Renewable and Sustainable Energy Reviews*, 14(9), 2841-2851.
- [46]Liu, L., et al. (2020). "Oxygen gasification of municipal solid waste in a fixed-bed gasifier." *Fuel*, 259, 116245.
- [47]Emami-Taba, L., et al. (2013). "Fuel blending effects on gasification process." *Energy & Fuels*, 27(2), 903-912.
- [48] Ahmed, S., & Gupta, A. K. (2010). "Syngas yield during CO<sub>2</sub> gasification of biomass." *Applied Energy*, 87(1), 87-92.
- [49] Kuo, P. C., et al. (2014). "Gasification performances of raw and torrefied biomass in a downdraft gasifier." *Energy Conversion and Management*, 87, 678-687.
- [50] Basu, P. (2010). *Biomass Gasification and Pyrolysis: Practical Design and Theory*. Elsevier.
- [51] Higman, C., & van der Burgt, M. (2008). *Gasification (2nd ed.)*. Gulf Professional Publishing.
- [52] Knoef, H. (Ed.). (2012). *Handbook of Biomass Gasification*. BTG Biomass Technology Group
- [53] Materazzi, M. (2017). *Gasification of Waste Materials*. Academic Press.
- [54]Akkache, S., Hernandez, A., Teixeira, G., & Gelix, F. (2016). Steam gasification of biomass in a fluidised bed of inert particles: Experiment and modelling. *Fuel Processing Technology*, 142, 98-106.
- [55]Lahijani, P., Zainal, Z. A., Mohammadi, M., & Mohamed, A. R. (2018). Conversion of the greenhouse gas CO<sub>2</sub> to the fuel gas CO via the Boudouard reaction: A review. *Renewable and Sustainable Energy Reviews*, 41, 615-632.

- [56] Patra, T. K., & Sheth, P. N. (2015). Biomass gasification models for downdraft gasifier: A state-of-the-art review. *Renewable and Sustainable Energy Reviews*, 50, 583-593.
- [57] Pinto, F., André, R., Miranda, M., Neves, D., Varela, F., & Santos, J. (2018). Effect of gasification agent on co-gasification of rice production wastes mixtures. *Fuel*, 180, 407-416.
- [58] Zhang, Y., Wang, Y., Cai, L., Yao, C., Gao, S., & Xu, G. (2019). Dual fluidized bed gasification of biomass with controlled char recirculation: Experimental study on process performance. *Energy*, 183, 1063-1073
- [59] Higman, C., & van der Burgt, M. (2008). *Gasification* (2nd ed.). Elsevier.
- [60] Rauch, R., et al. (2014). *Biomass Gasification for Synthesis Gas Production and Applications of the Syngas*. Wiley.
- [61] Woolcock, P. J., & Brown, R. C. (2013). *A review of cleaning technologies for biomass-derived syngas*. *Biomass and Bioenergy*, 52, 54-84.
- [62] Rostrup-Nielsen, J. R. (2002). *Syngas in Perspective*. *Catalysis Today*, 71(3-4), 243-247.
- [63] Liu, K., et al. (2011). *Comparison of biomass gasification technologies for hydrogen production*. *Energy & Fuels*, 25(10), 4679-4686.
- [64] Spath, P. L., & Dayton, D. C. (2003). *Preliminary Screening of Technical and Economic Feasibility of Biomass Gasification for Power Generation*. NREL.
- [65] Dry, M. E. (2002). \*The Fischer-Tropsch Process: 1950–2000\*. *Catalysis Today*, 71(3-4), 227-241.
- [66] IPCC (2018). *Global Warming of 1.5°C – Special Report on Carbon Capture Utilization and Storage*.
- [67] Zhang, Y., et al. (2020). *Advances in catalytic gasification for hydrogen-rich syngas production*. *Renewable and Sustainable Energy Reviews*, 134, 110340.
- [68] Speight, J. G. (2018). *Handbook of Natural Gas Analysis*. Wiley.
- [69] Higman, C., & van der Burgt, M. (2008). *Gasification* (2nd ed.). Elsevier.

## References

---

- [70] EPA (Environmental Protection Agency). (2020). *Air Pollution Control Technology Fact Sheets*.
- [71] Mokhatab, S., et al. (2019). *Handbook of Natural Gas Transmission and Processing*. Gulf Professional Publishing.
- [72] US EPA (2022, 2023) – Emission standards and combustion sources.
- [73] WHO (2021) – Air quality guidelines.
- [74] IPCC (2006) – Industrial emission factors.
- [75] European Environment Agency (2020) – Waste incineration data.
- [76] III.3.3. Calorific value of the gas
- [77] U.S. Energy Information Administration (EIA) – Natural Gas Heat Content.
- [78] International Energy Agency (IEA) – Natural Gas Standards.
- [80] Engineering ToolBox – Methane Combustion Data.
- [81] National Institute of Standards and Technology (NIST) – Thermodynamic Properties.
- [82] LPGas Magazine – Propane & Butane Energy Content.
- [83] World LPG Association (WLPGA) – LPG Specifications.
- [84] U.S. Department of Energy (DOE) – Hydrogen Fuel Basics.
- [85] European Hydrogen Association (EHA) – Hydrogen Energy Metrics.
- [86] International Renewable Energy Agency (IRENA) – Biogas Potential.
- [87] American Biogas Council – Biogas Composition & Energy.
- [88] Misra, M. K., Ragland, K. W., & Baker, A. J. (1993). *Wood ash composition as a function of furnace temperature*. *Biomass and Bioenergy*, 4(2), 103-116.
- [89] Etiegni, L., & Campbell, A. G. (1991). *Physical and chemical characteristics of wood ash*. *Bioresource Technology*, 37(2), 173-178.
- [90] American Coal Ash Association (ACAA). (2020). *Coal Combustion Product (CCP) Production & Use Survey Report*.

## References

---

- [91]Ahmaruzzaman, M. (2010). *A review on the utilization of fly ash*. Progress in Energy and Combustion Science, 36(3), 327-363.
- [92] Chandrasekhar, S., et al. (2003). *Review on processing, properties and applications of reactive silica from rice husk ash*. Materials Science and Engineering, 36(1), 59-65.
- [93] Sabbas, T., et al. (2003). *Management of incinerator residues*. Waste Management, 23(1), 61-88.
- [94] Fisher, R. V., & Schmincke, H. U. (1984). *Pyroclastic Rocks*. Springer-Verlag.
- [95]Vassilev, S. V., & Vassileva, C. G. (2007). *A new approach for the classification of coal fly ashes based on their origin, composition, properties, and behaviour*. Fuel, 86(10-11), 1490-1512.
- [96]hy, P., Jenkins, B. M., Grundvig, S., Shiraki, R., & Leshner, C. E. (2013). *High temperature elemental losses and mineralogical changes in common biomass ashes*. Fuel, 106, 301-312.
- [97]Sarbak, Z., & Kramer-Wachowiak, M. (2002). *Characterization of coal fly ashes by SEM-EDS*. Mikrochimica Acta, 139(1-4), 137-142.
- [98]Yao, Z. T., Ji, X. S., Sarker, P. K., Tang, J. H., Ge, L. Q., Xia, M. S., & Xi, Y. Q. (2015). *A comprehensive review on the applications of coal fly ash*. Earth-Science Reviews, 141, 105-121.
- [100]Chandrasekhar, S., Pramada, P. N., & Majeed, J. (2003). *Effect of calcination temperature and heating rate on the optical properties and reactivity of rice husk ash*. Journal of Materials Science, 41(23), 7926-7933.
- [101]Basu, P. (2010). *Biomass Gasification and Pyrolysis: Practical Design and Theory*. Academic Press.  
(Covers material/energy balances in gasification systems.)
- [102]Higman, C., & van der Burgt, M. (2008). *Gasification (2nd ed.)*. Gulf Professional Publishing.  
(Detailed discussion on gasification thermodynamics.)

## References

---

- [103]Kumar, A., Jones, D. D., & Hanna, M. A. (2009). *Thermochemical Biomass Gasification: A Review*. *Renewable and Sustainable Energy Reviews*, 13(1), 179-186. (Review of gasification reactions and efficiencies.)
- [104]Zainal, Z. A., et al. (2001). *Prediction of Performance of a Downdraft Gasifier Using Equilibrium Modeling*. *Fuel*, 80(5), 683-689. (Equilibrium models for gasification material balance.)
- [105]Ptasinski, K. J. (2016). *Efficiency of Biomass Energy: An Exergy Approach*. Wiley. (Energy and exergy analysis of gasification.)
- [106]International Energy Agency (IEA) Renewables Reports
- [107]BloombergNEF (BNEF) Energy Finance
- [108] IPCC (2021). *Climate Change 2021: The Physical Science Basis*. [Link](#)
- [109]Tian et al. (2020). *Nature Climate Change*, "A comprehensive quantification of global nitrous oxide sources and sinks." DOI:10.1038/s41558-020-0722-3
- [110]EPA (2023). *Inventory of U.S. Greenhouse Gas Emissions and Sinks*. [Link](#) UNEP (2019). *Global Mercury Assessment*. [Link](#)
- [111]USGS (2020). *Nutrient Pollution*. [Link](#)
- [112]GESAMP (2019). *Sources, Fate and Effects of Microplastics in the Marine Environment*. [Link](#)
- [113] Appels, L., et al. (2011). *Renewable and Sustainable Energy Reviews*, 15(1), 4295-4301
- [114] Bridgwater, A. V. (2012). *Biomass and Bioenergy*, 38, 68-94.
- [115] McKendry, P. (2002). *Bioresource Technology*, 83(1), 55-63.
- [116] Libra, J. A., et al. (2011). *Biofuels*, 2(1), 71-106.